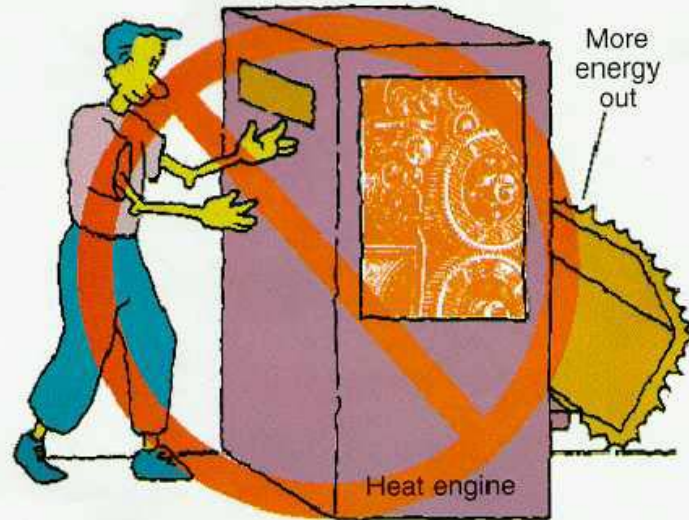
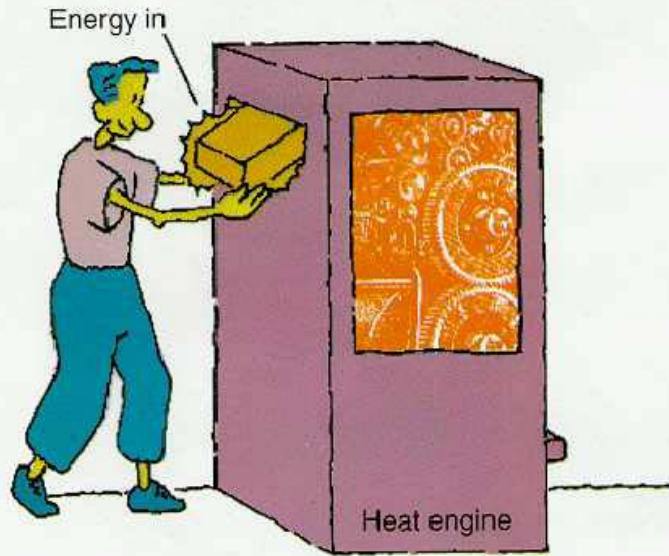


The Second Law of Thermodynamics

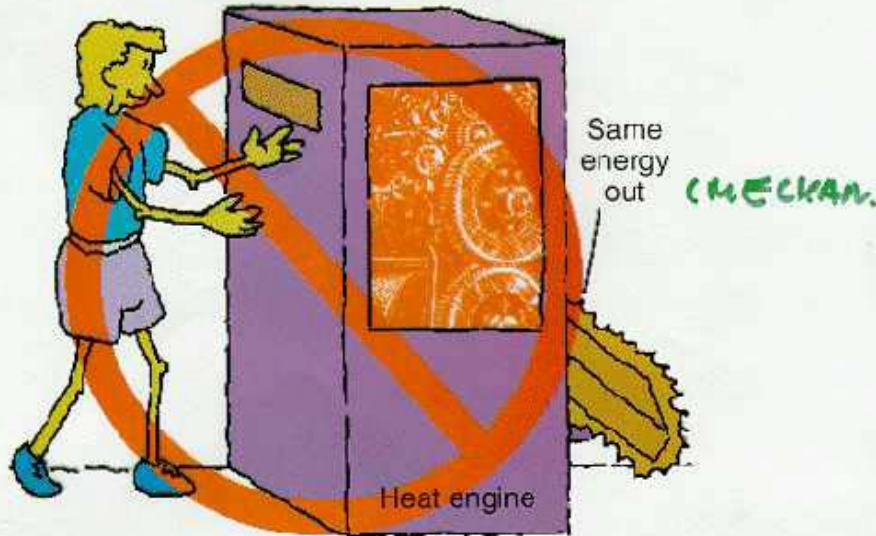
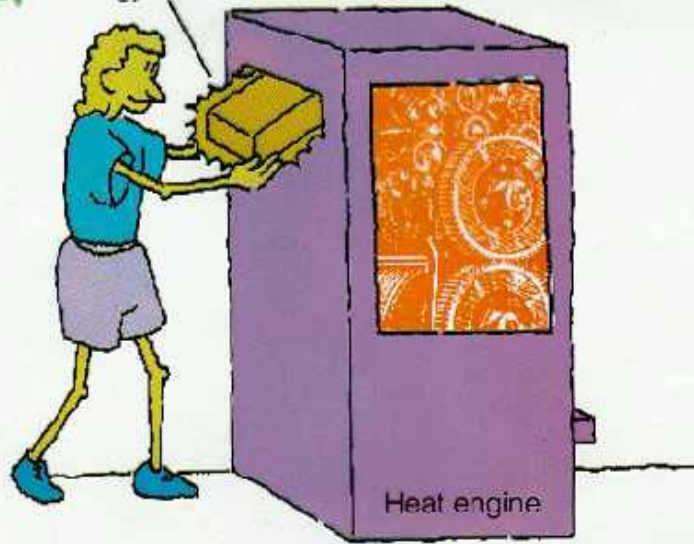
The First Law of Thermodynamics

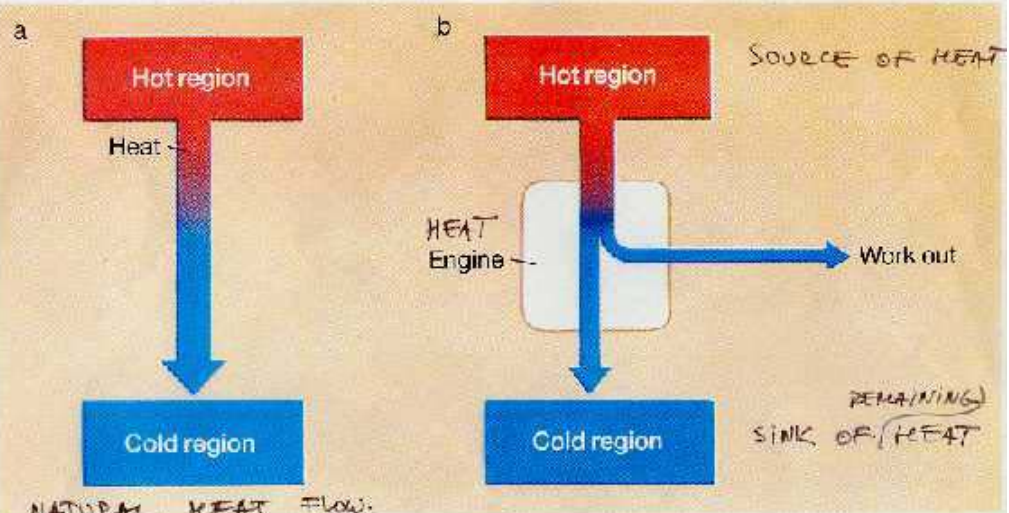


The Second Law of Thermodynamics

HEAT

Energy in





NATURAL HEAT FLOW:

HOT → COLD;
IRREVERSIBLE
PROCESS

(a) Heat naturally flows from a higher temperature region to a lower temperature region.
(b) A heat engine extracts part of the thermal energy to perform mechanical work and exhausts the remaining thermal energy.

26. Figure 10.6. (Kirkpatrick/Wheeler)

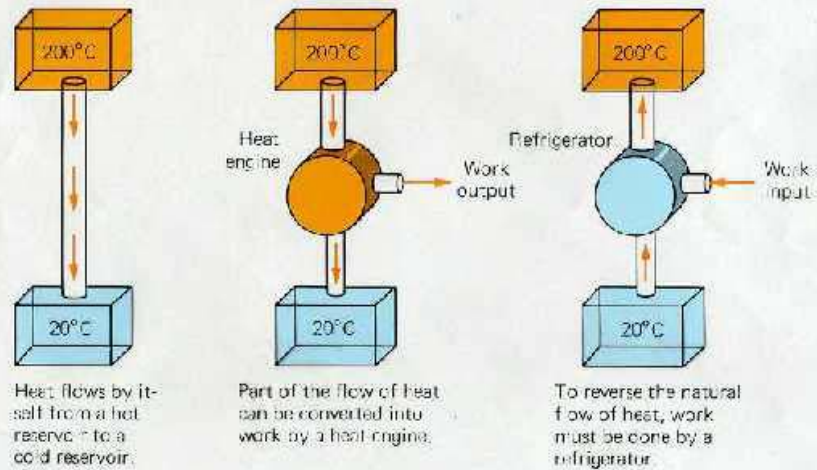
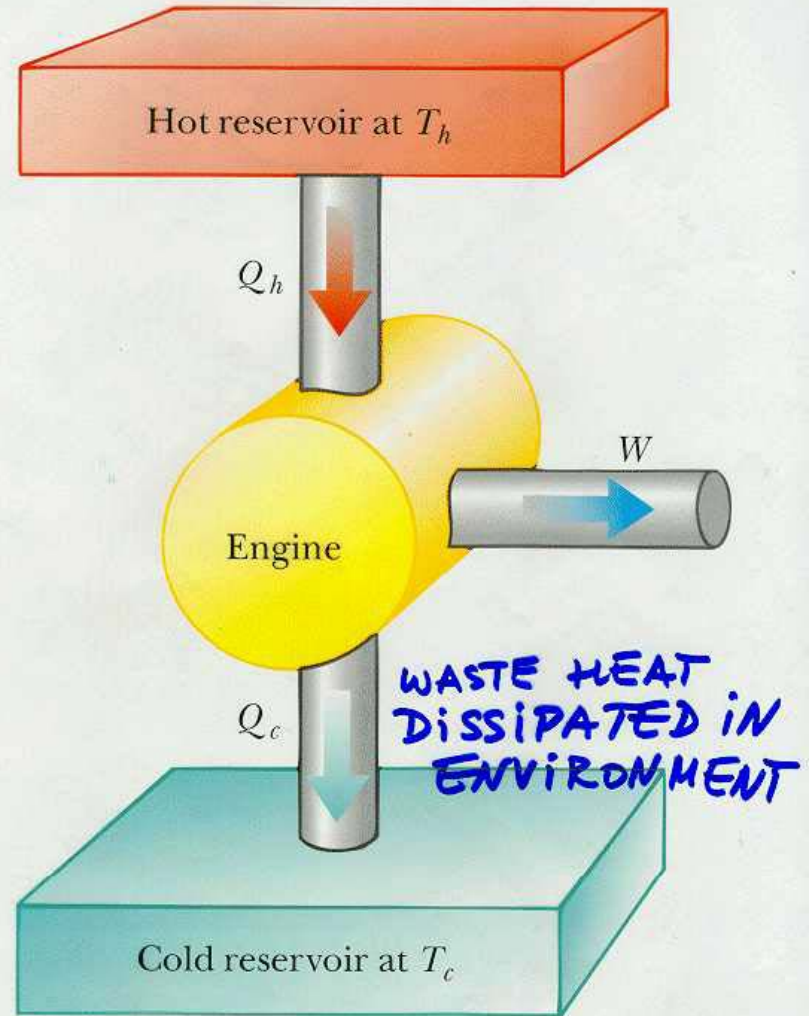
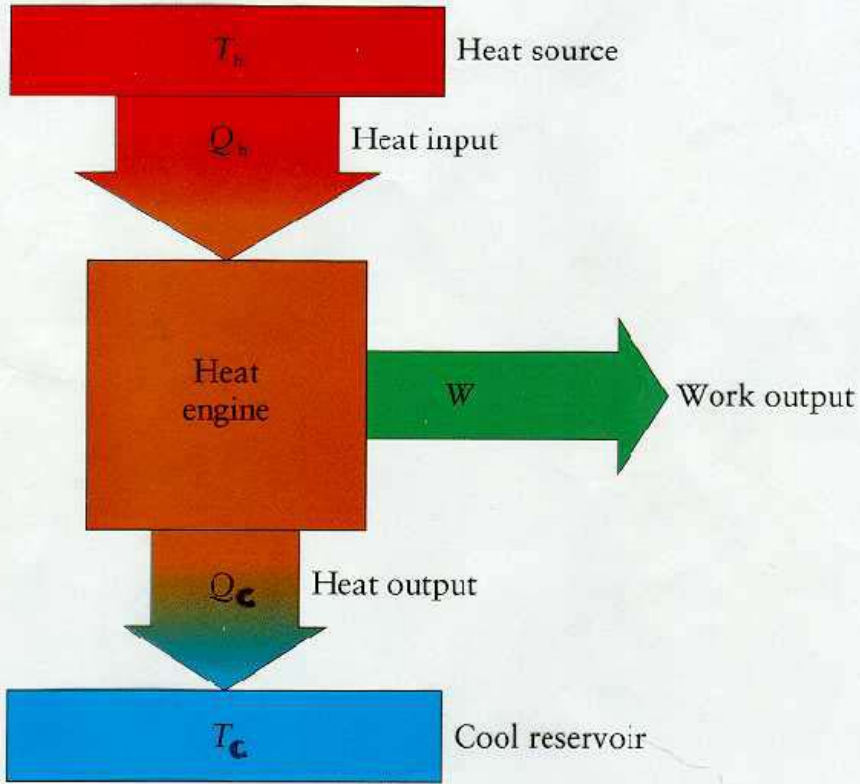


Diagram of a Heat Engine



6)

Transparency 58

Figure 16.14 Page 664

A Heat Engine

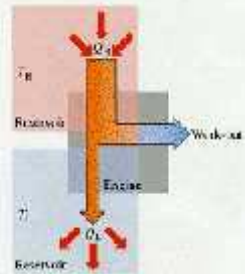


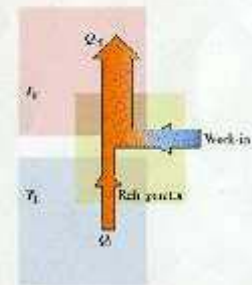
Figure 16.19 Page 666

A Waterfall Analogy for a Heat Engine



Figure 16.22 Page 667

A Refrigeration Machine





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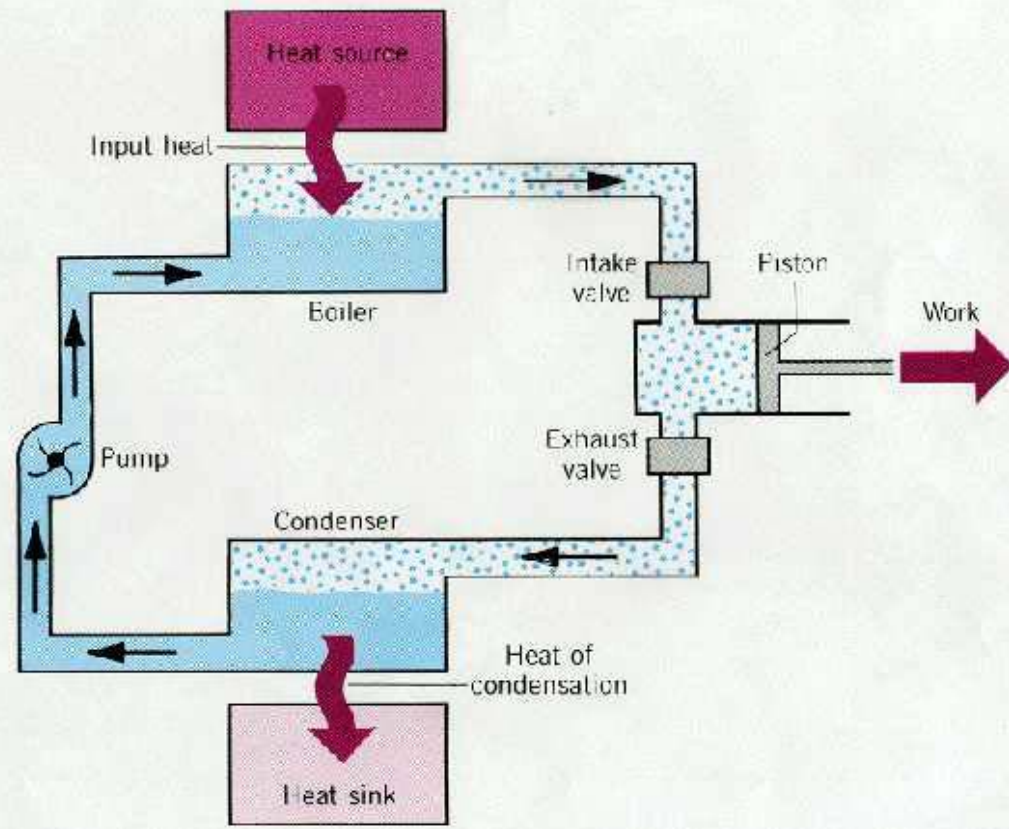
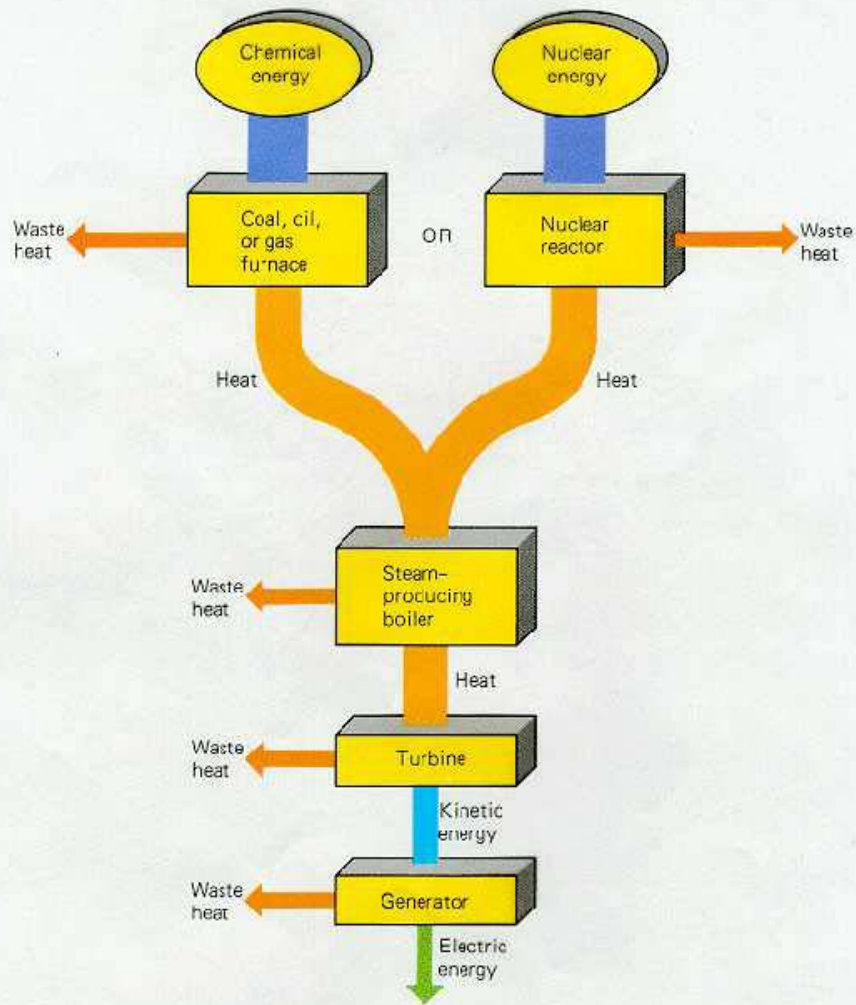
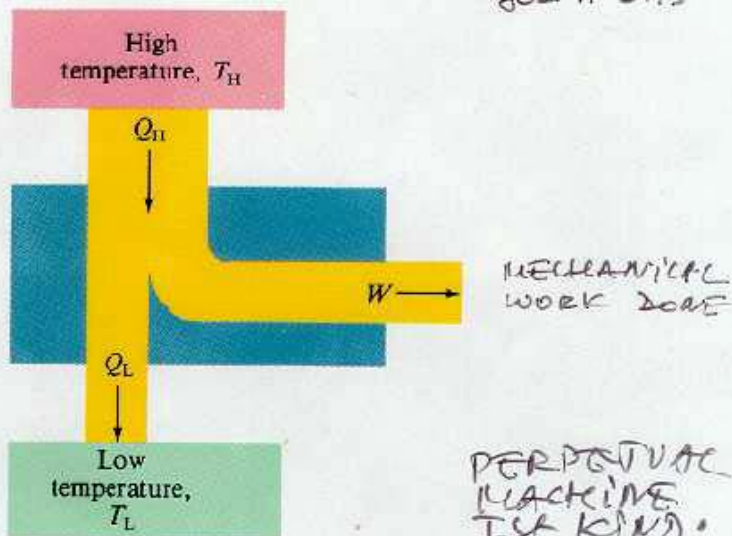
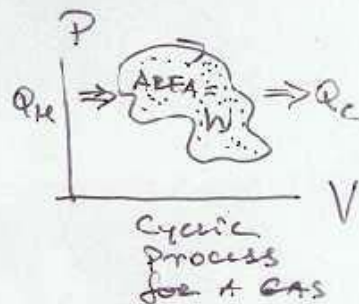


FIGURE 15.11 131



71)

FIGURE 15-6 Schematic diagram of a heat engine.



PERPETUAL MACHINE 1st KIND: $\emptyset \rightarrow \text{ENERGY}$

A WORKING SUBSTANCE (AIR-FUEL MIXTURE, STEAM, ETC.) IS CARRIED THROUGH A CYCLIC PROCESS AND RETURNS TO THE INITIAL STATE AFTER EVERY CYCLE:

$$\Delta U_{\text{cycle}} = 0 \Rightarrow \text{1st LAW: } Q_{\text{NET}} = W,$$

$$Q_{\text{NET}} = Q_H - |Q_C|, \text{ AND}$$

$$\Delta U = Q - W$$

$$Q_H = W + Q_C$$

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ENERGY CONSERV.

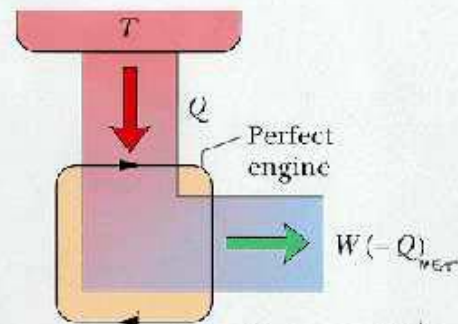
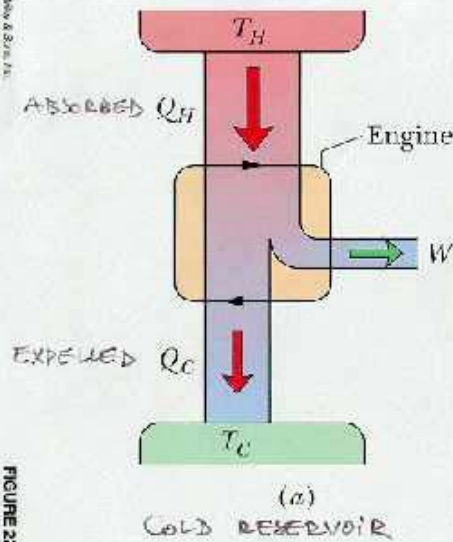
9)

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THERMAL EFFICIENCY

$$e \equiv \frac{W}{Q_H} = \frac{Q_H - Q_C}{Q_H} = 1 - \frac{Q_C}{Q_H} < 1$$

for $Q_C \neq 0$.

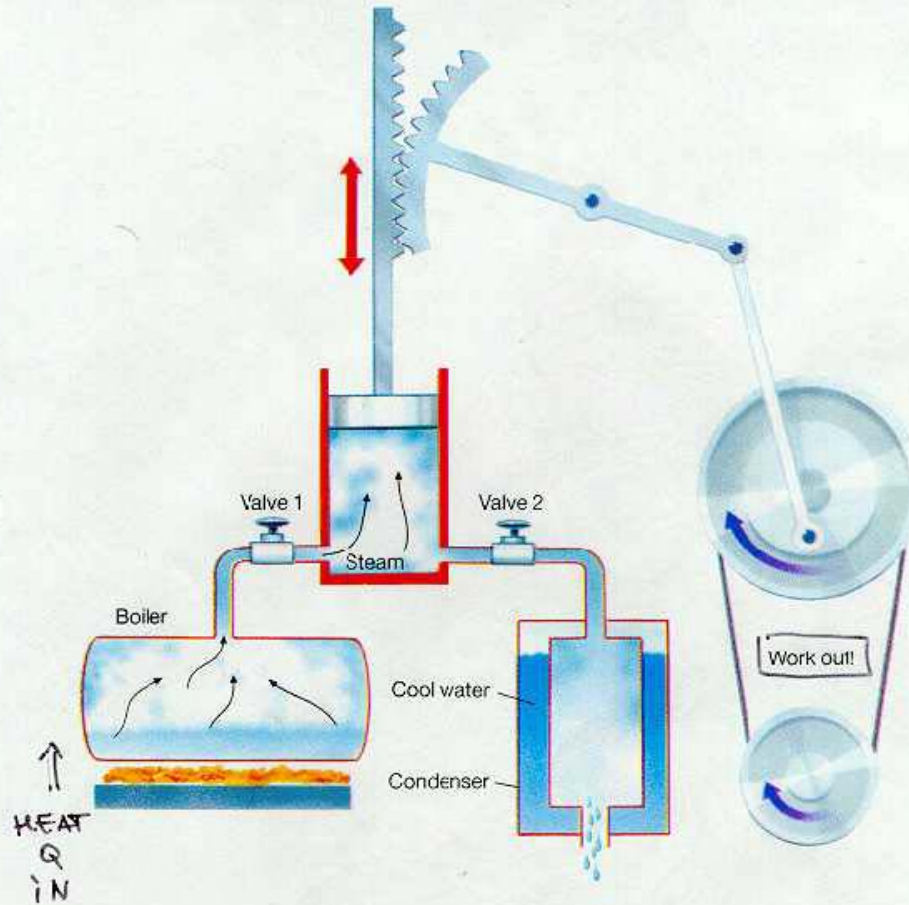


$e_{\text{CAR}} \approx 20\%$, $e_{\text{DIESEL}} \approx 35\%$, etc.
 \Rightarrow ALL HEAT ENGINES
 HAVE $e < 1$, or $e < 100\%$

II LAW OF THERMODYNAMICS:
 IT IS IMPOSSIBLE TO CONSTRUCT
 A CYCLIC HEAT ENGINE CON-
 VERTING ALL ITS ABSORBED
 THERMAL ENERGY INTO WORK:
 $e < 1$

FIGURE 22.2 76

THE WATT'S STEAM ENGINE

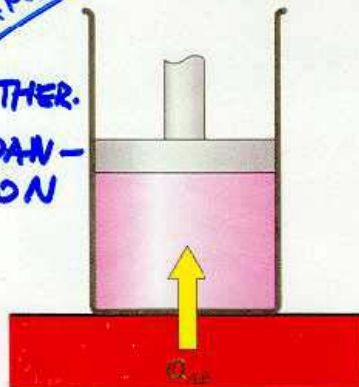


The essential features of Watt's steam engine.

10)

THE PHYSICS TEACHER'S CYCLE

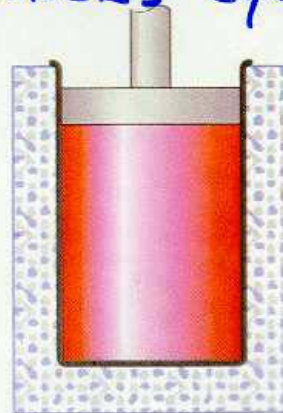
EXAMPLE
ISOTHER.
EXPAN-
SION



$$T_A = T_B = 19.2 \text{ K}$$

(a)

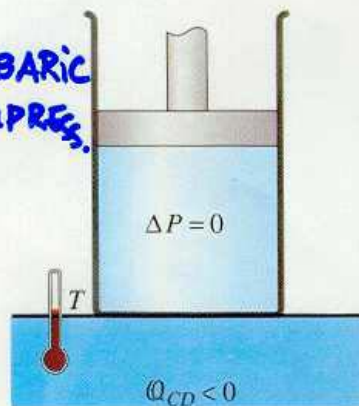
ADIAB.
EXPAN.



$$(Q_{BC} = 0)$$

(b)

ISOBARIC
COMPRES.

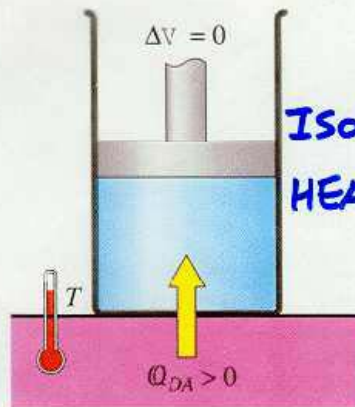


$$\Delta P = 0$$

$$Q_{CD} < 0$$

(c)

ISOVOLUME
HEATING



$$\Delta V = 0$$

$$Q_{DA} > 0$$

(d)

FIND P_B, V_B : ON BC (ADIAB.) $P_B V_B^\gamma = P_C V_C^\gamma$

AT B: $P_B V_B = nRT_B$

2 EQS FOR
2 UNKNOWNS:

$P_B = 3.51 \times 10^4 \text{ PA}$

$V_B = 4.55 \times 10^{-3} \text{ m}^3$

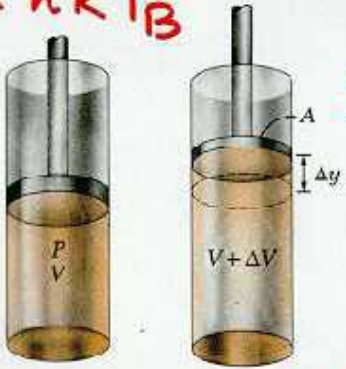


Fig. 13-1

He: $f=3$

$\gamma = 5/3$

$C_V = \frac{f}{2} R = \frac{3}{2} R = 12.5 \frac{\text{J}}{\text{mol} \cdot \text{K}}$

$C_P = C_V + R = 20.8 \frac{\text{J}}{\text{mol} \cdot \text{K}}$

We now have P, V, T AT EACH VERTEX.

FIND $Q, W, \Delta U$:

ISOTHERM $A \rightarrow B$:

$W_{AB} = nRT_A \ln \frac{V_B}{V_A}$
 $= 1 \times 8.3 \times 19.2 \times \ln \frac{4.55}{2}$
 $= 132 \text{ J};$

$\Delta U_{AB} = 0$, SO
 (1ST LAW: $0 = Q - W$)

$Q_{AB} = W_{AB} = 132 \text{ J}$

ADIABAT $B \rightarrow C$:

$Q_{BC} = 0$;

$\Delta U_{BC} = nC_V(T_C - T_B)$
 $= 1 \times 12.5 \times (18 - 19.2)$
 $= -15 \text{ J};$

1ST LAW: $\Delta U = 0 - W$

$W_{BC} = +15 \text{ J}$

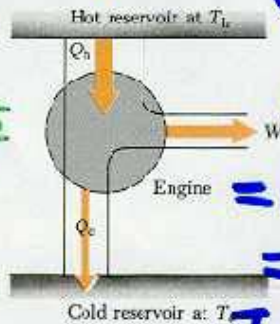
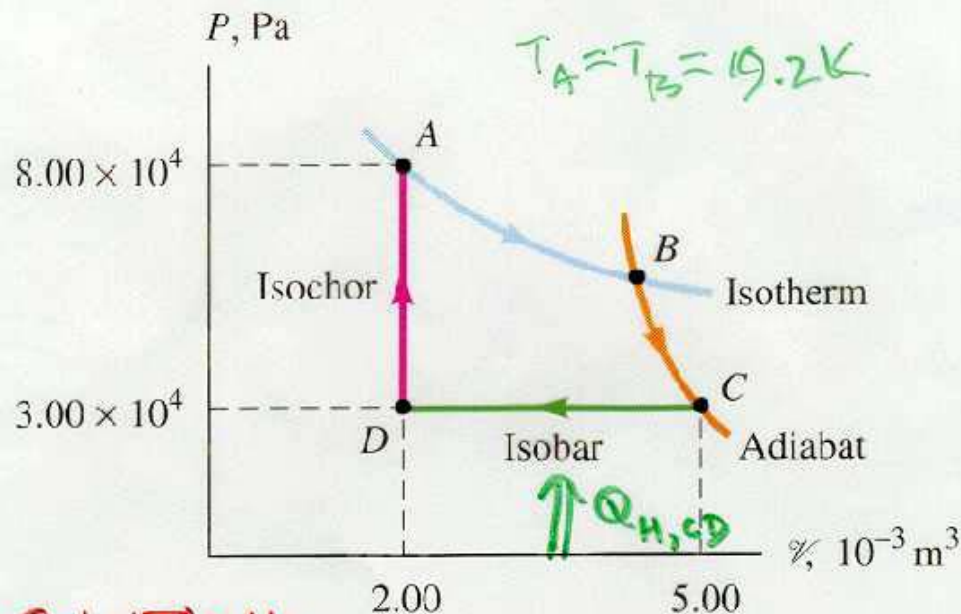


Fig. 13-6

COMPUTE ΔU , Q AND W FOR EACH PORTION OF THE CYCLE AND THEIR TOTALS FOR THE CYCLE

GIVEN: $P_A, P_D = P_C, V_A = V_D, V_C$

1 MOLE OF HELIUM (IDEAL), monatomic



SOLUTION:

$$T_B = T_A = \frac{P_A V_A}{nR} = \frac{8 \times 10^4 \text{ Pa} \times 2 \times 10^{-3} \text{ m}^3}{1 \text{ MOLE} \times 8.3 \text{ J/MOLE} \cdot \text{K}} = 19.2 \text{ K}$$

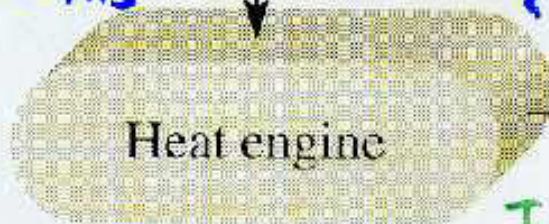
SIMIL. $T_C = P_C V_C / nR = 18.0 \text{ K}$

$T_D = P_D V_D / nR = 7.22 \text{ K}$

25/10/17



$Q_{DA} + Q_{AB} = 150 + 132 = 282 \text{ J}$



$Q_{CD} = 225 \text{ J}$



ISOBAR C \rightarrow D:

$W_{CD} = P_C (V_D - V_C) =$
 $= 3 \cdot 10^4 \text{ Pa} (2 \cdot 10^{-3} \text{ m}^3 - 5 \cdot 10^{-3} \text{ m}^3)$
 $= -90 \text{ J}$

$Q_{CD} = n C_p \Delta T = n \cdot \frac{5}{2} R (T_D - T_C)$
 $= 1 \text{ mol} \times 20.8 \frac{\text{J}}{\text{mol} \cdot \text{K}} \times (7.2 - 18) \text{ K}$
 $= -225 \text{ J}$

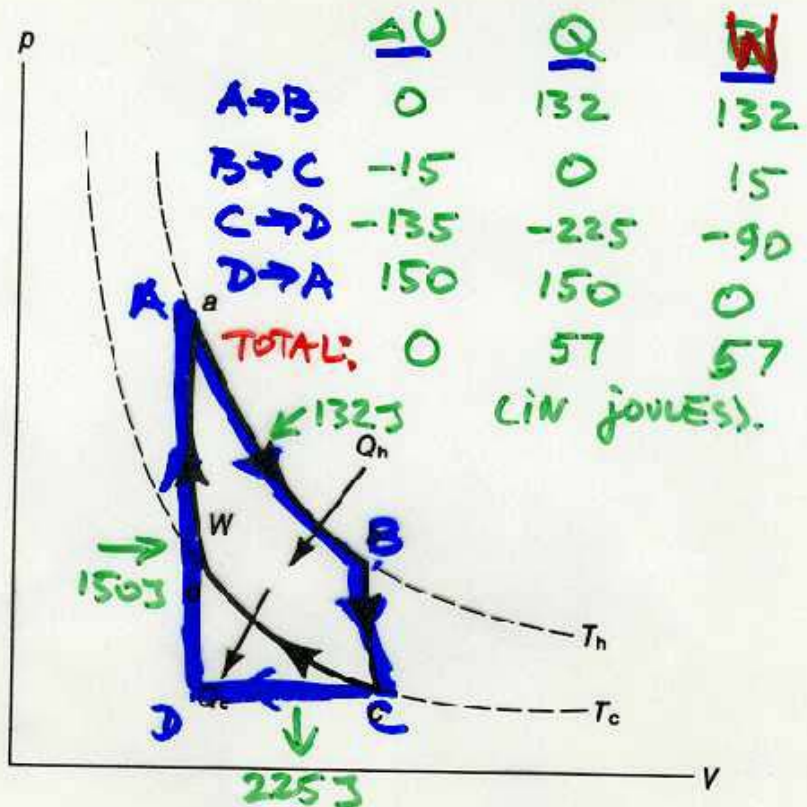
Work (57 J)

I LAW: $\Delta U_{CD} = Q_{CD} - W_{CD} =$
 $= (-225 \text{ J}) - (-90 \text{ J}) = -135 \text{ J}$

ISOCOR D \rightarrow A:

$W_{DA} = 0 \quad (V = \text{CONST})$
 I LAW: $\Delta U_{DA} = Q_{DA} - 0 =$
 $= n C_v (T_A - T_D) = n \cdot \frac{3}{2} R \cdot \Delta T$
 $= 1 \text{ mol} \times 12.5 \text{ J/mol} \cdot \text{K} \times (19.2 - 7.2) = 150 \text{ J}$

SUMMARY:



Efficiency:

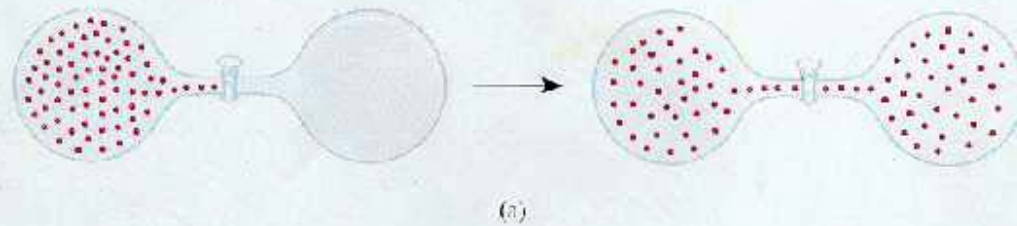
Figure 22-7

$$e = \frac{W}{Q_h} = \frac{W(\text{cycle})}{Q_{AB} + Q_{DA}} = \frac{57}{132 + 150} = \frac{57}{282} \approx 0.20 = 20\%$$

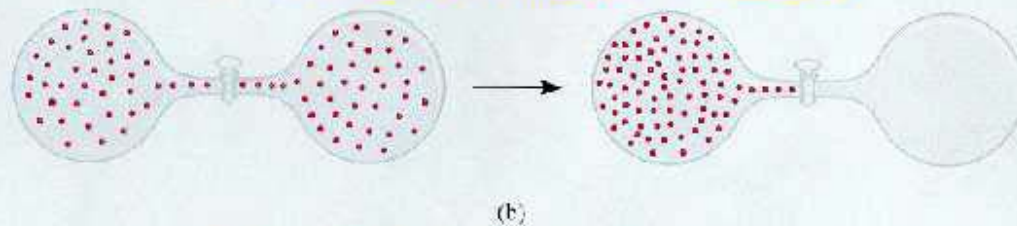
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30) 10%

A SPONTANEOUS PROCESS



A NON-SPONTANEOUS PROCESS

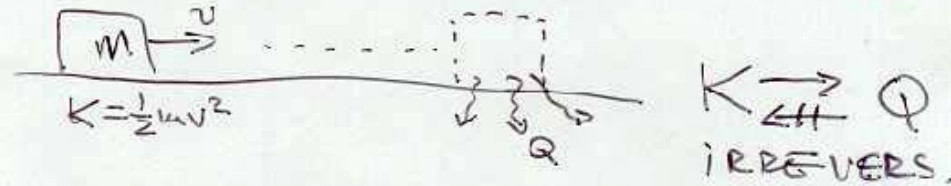


IRREVERSIBLE

EACH ELASTIC COLLISION CAN BE RUN BACKWARDS AS AN EQUALLY POSSIBLE PROCESS; BUT THE CHANCE OF THE MOLECULES TO SPONTAN. COLLECT IN LEFT TANK ≈ 0 .

PHYSICAL PROCESSES: → IRREVERSIBLE

→ REVERSIBLE

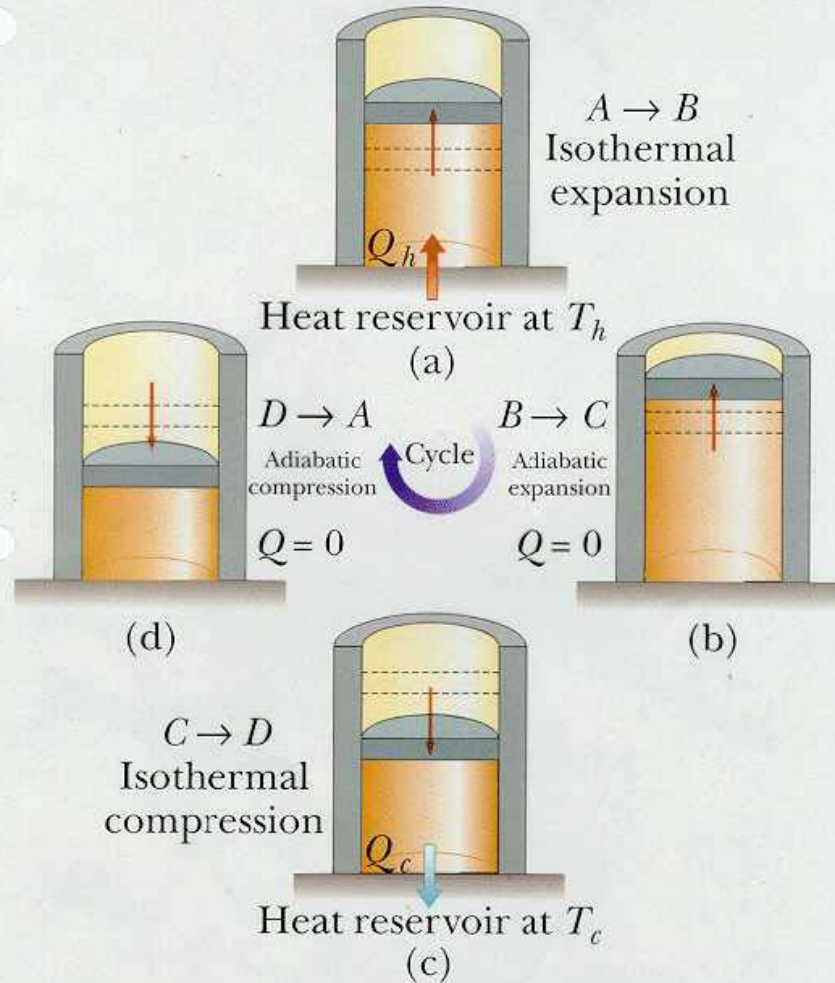


REVERSIBLE:

- * QUASI-STATIC (EQUIL. STATES)
- * NO DISSIPATION OF MECH. ENERGY TO HEAT (NEGLECTIBLE FRICTION)
- * NO HEAT CONDUCTION WITH FINITE $\Delta T \neq 0$

CAN BE REPRESENTED ON P-V DIAGRAM; IRREVERSIBLE - CAN NOT (NO DEFINITE UNIQUE P).

THE CARNOT CYCLE

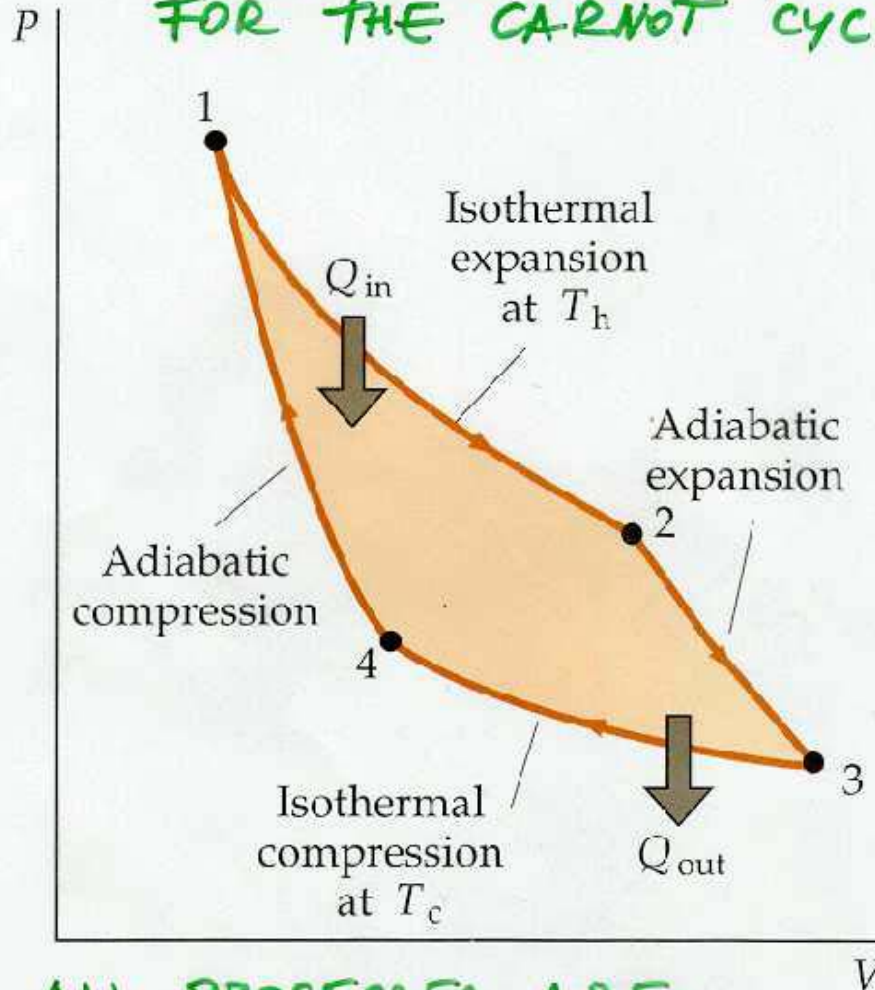


Overhead transparencies to accompany Serway/Faughn: *College Physics, 4/e*
Figure 60 Text figure 12.10

page 365

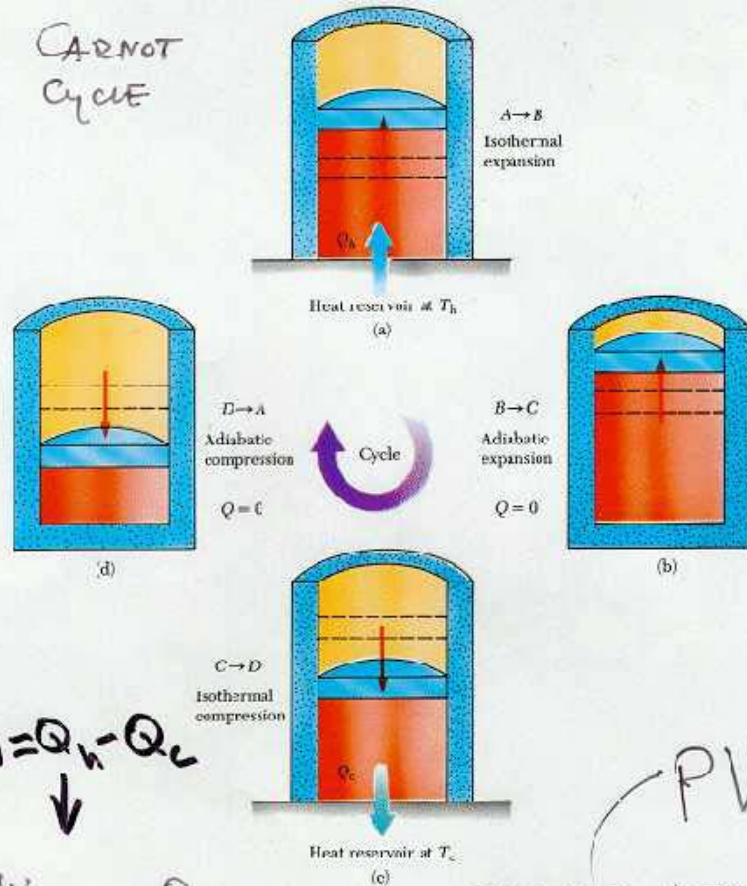
13) The Carnot cycle

THE P-V DIAGRAM FOR THE CARNOT CYCLE



ALL PROCESSES ARE REVERSIBLE

CARNOT Cycle

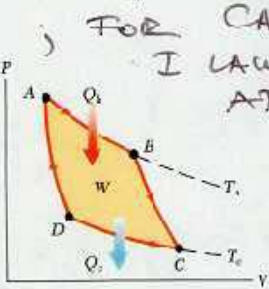


$$W = Q_h - Q_c$$

$$e = \frac{W}{Q_h} = 1 - \frac{Q_c}{Q_h}$$

↑
I LAW

$$PV^\gamma = \text{const}$$



FOR CARNOT (USING I LAW, IDEAL GAS AND ADIABATIC EQS)

$$\frac{Q_c}{Q_h} = \frac{T_c}{T_h} \Rightarrow$$

$$e_{\text{CARNOT}} = 1 - \frac{T_c}{T_h}$$

EXAMPLE:

PV CARNOT DIAGRAM

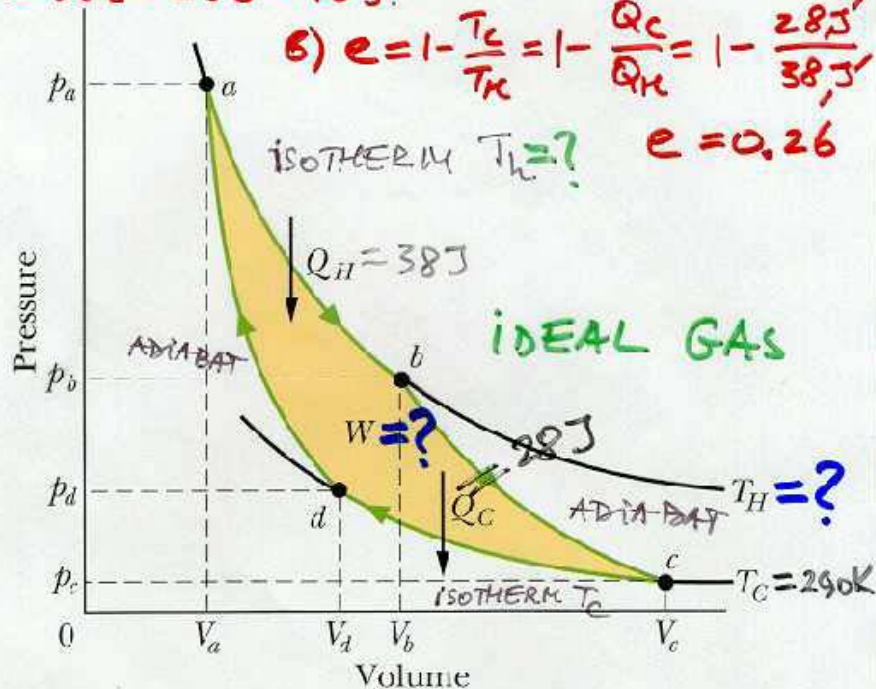
FIND WORK, EFFICIENCY AND T_H .

a) $W = \oint P dV$ OR 1ST LAW: $0 = (Q_H - Q_C) - W$

$W = 38\text{J} - 28\text{J} = 10\text{J}$.

b) $e = 1 - \frac{T_C}{T_H} = 1 - \frac{Q_C}{Q_H} = 1 - \frac{28\text{J}}{38\text{J}}$

ISOTHERM $T_H = ?$ $e = 0.26$



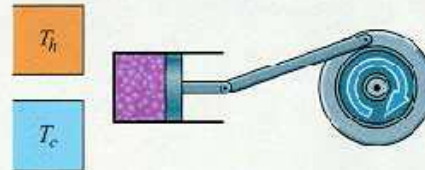
c) $e = 1 - \frac{T_C}{T_H} \Rightarrow e - 1 = -T_C/T_H \Rightarrow$

$T_H(1 - e) = T_C \Rightarrow T_H = \frac{T_C}{1 - e} =$

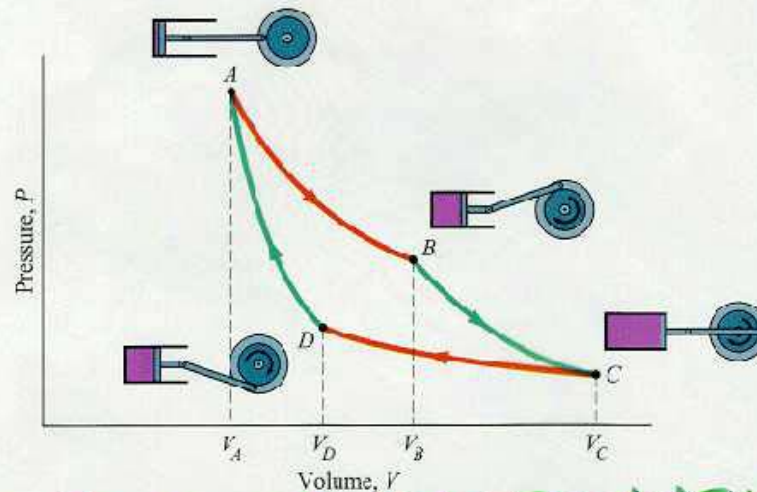
$= \frac{290\text{K}}{1 - 0.26} = 390\text{K}$

16)

THE IMPORTANCE OF THE CARNOT ENGINE T-50



1. $e = 1 - T_c/T_h$, EVEN IF GAS IS NOT IDEAL - ANY FLUID CAN BE USED; OTHERWISE, II LAW WOULD BE VIOLATED.



2. IT IS THE MOST EFFICIENT ENGINE POSSIBLE OPERATING BETWEEN GIVEN T_h, T_c

CARNOT ENGINE AS THERMOMETER:

IDEAL GAS TEMP. SCALE:

V = CONST GAS THERMOMETER

$$T = \lim_{n \rightarrow 0} \frac{P}{P_3} 273.16$$

WITH THE CARNOT ENGINE RUN BETWEEN A SYSTEM OF UNKNOWN TEMP. T AND A TRIPLE CELL OF WATER WITH ITS TEMP. DEFINED TO BE $T_2 = 273.16$, WE CAN USE THE RELATION

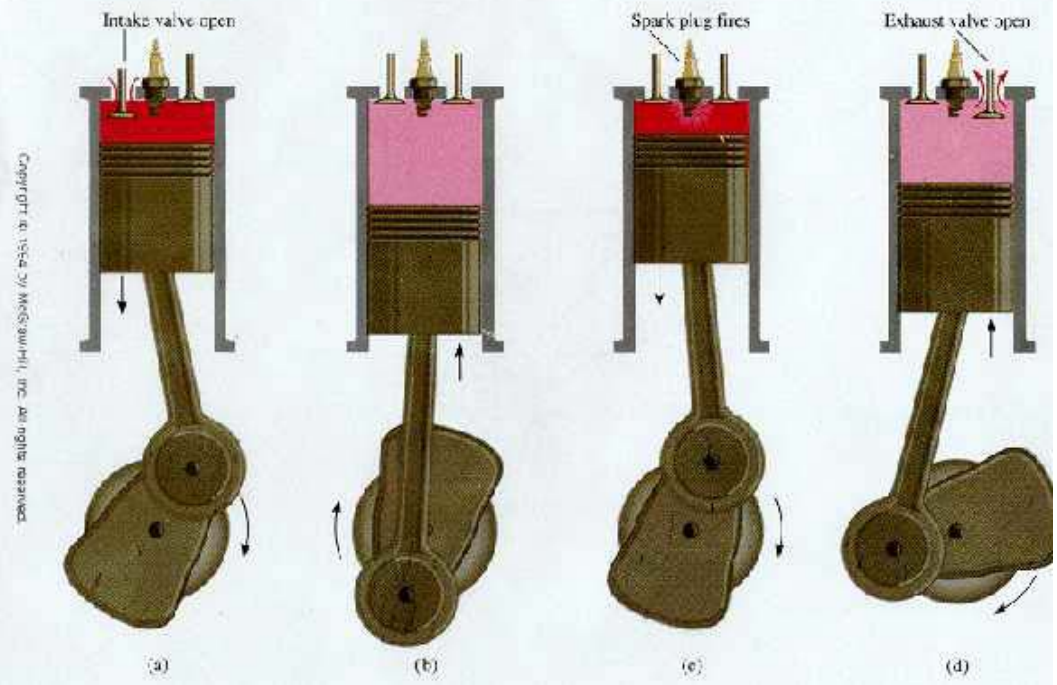
$$\frac{T}{T_2} = \frac{Q_1}{Q_2} \quad \text{TO DEFINE}$$

ABSOLUTE TEMP. SCALE

$$T \stackrel{\text{DEF}}{=} 273.16 \text{ K} \frac{Q_1}{Q_2}$$

INDEP. OF WORKING SUBSTANCE,
VALID AT V. LOW TEMP. ERAP.
(WHERE GASES LIQUIFY).
FINAL (ULTIMATE) THERMOMETER! CARNOT ENGINE!

INTERNAL COMBUSTION ENGINE



201

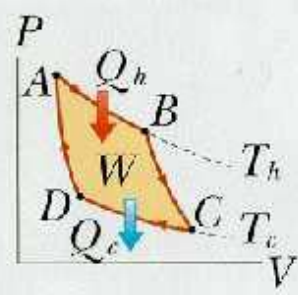


Figure 22.9

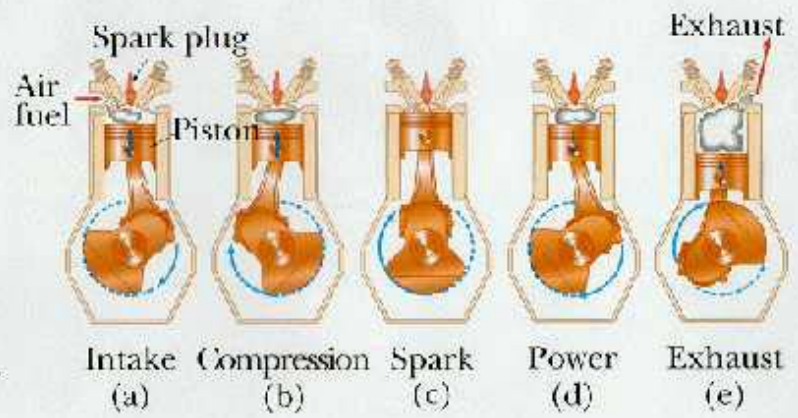


Figure 22.10

21)

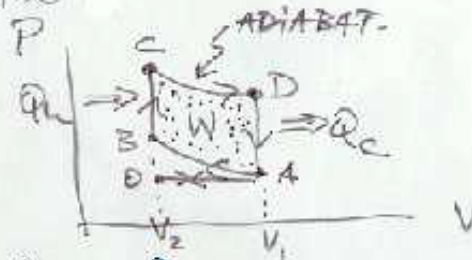
GASOLINE ENGINE

OTTO CYCLE:

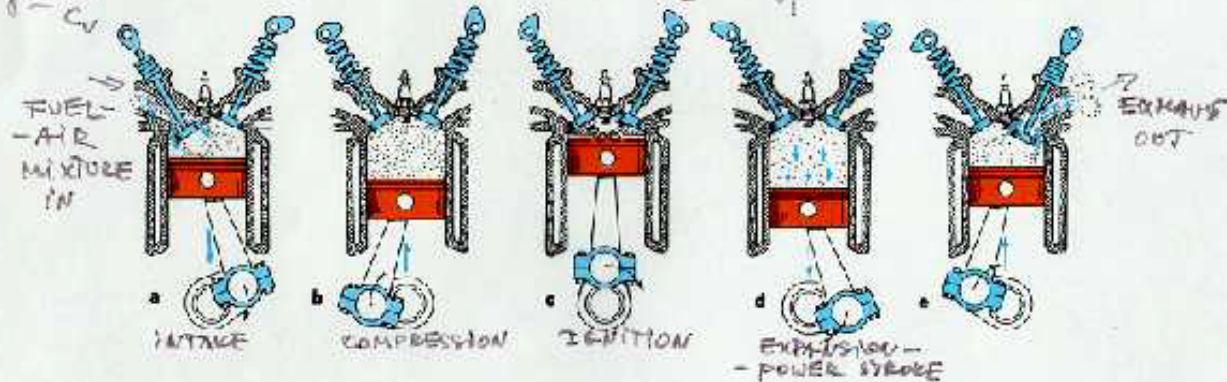
T-33

$$\epsilon = 1 - \frac{1}{(V_1/V_2)^{\gamma-1}}$$

$$\gamma = \frac{C_p}{C_v}$$



V_1/V_2 COMPRESS. RATIO



A FOUR-CYCLE INTERNAL COMBUSTION ENGINE

FOR $V_1/V_2 \approx 8$ & $\gamma_{AIR} = 1.4$, $\epsilon_{THEOR} = 56\%$

DISEL: $V_1/V_2 \approx 16$

$\epsilon_{REAL} \approx 15\text{ TO }20\%$

Figure 17.5
Conceptual Physics, Seventh Edition, by Paul G. Hewitt
Copyright © 1993 HarperCollins College Publishers

(FRICTION, INCOMPLETE COMBUSTION, HEAT LOSS)

WHY IS THERE $\eta < 1$,
EVEN IF WE ELIMINATED FRICTION?

REASON: WE NEED A CYCLIC, REPE-
TITIVE PROCESS OF CONVERSION $Q \rightarrow W$.
IN (c) GAS/AIR MIXTURE EXPLODES,
DRIVING THE PISTON DOWN. THIS COULD
BE 100% EFFICIENT, E.G. VIA ISOTHERM
PROCESS.

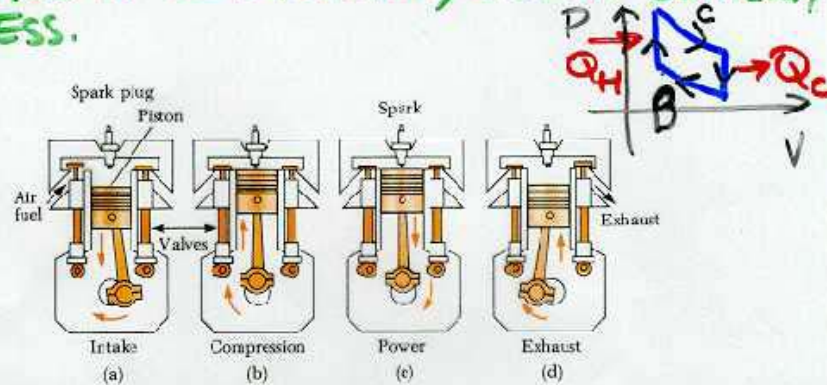


Fig. 13-8

BUT THE PISTON HAS TO BE RETURNED
TO THE TOP IN (b) TO PREPARE FOR
THE NEXT CYCLE, TO KEEP CAR
GOING. YOU HAVE TO COOL THE
CYLINDER, OTHERWISE IN COMPRES-
SION (b) YOU WOULD FINISH THE
CYCLE AT A HIGHER TEMPERATURE
THAN IT HAD AT THE BEGINNING.

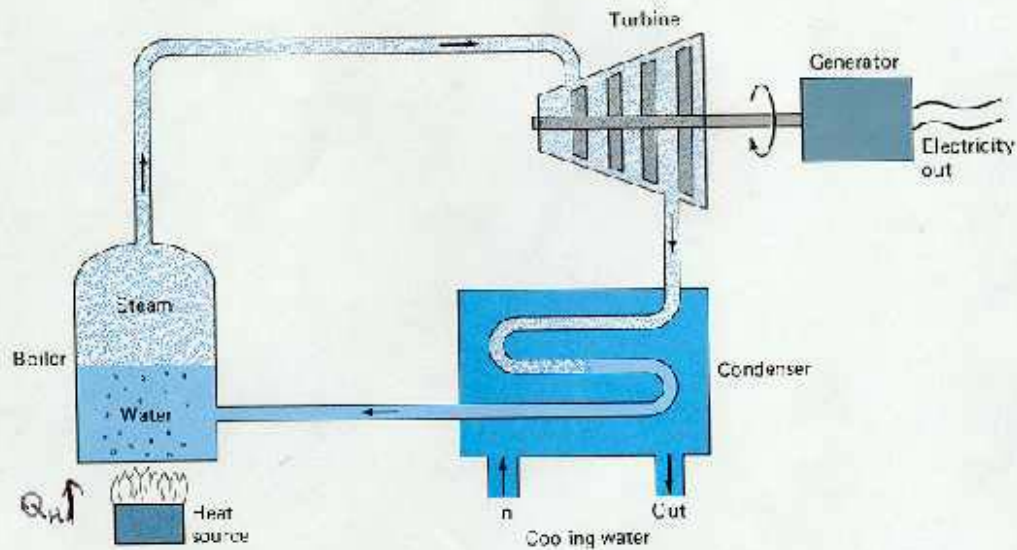
$\eta < 1$ THIS HEAT IS CARRIED AWAY BY
22) THE COOLING SYSTEM/RADIATOR.

14

Transparency 14 (Fig. 19-16)

Physics: Extended with Modern Physics by Wolfson and Pasachoff.

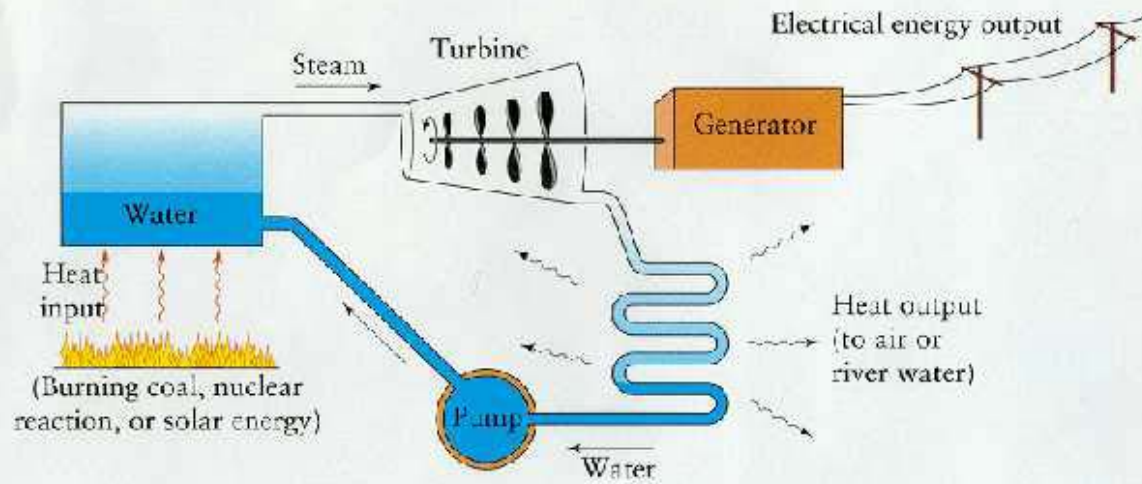
THERMAL POWER PLANT: HEAT TO ELECTRICITY



FUEL: COAL
GAS
OIL
NUCLEAR

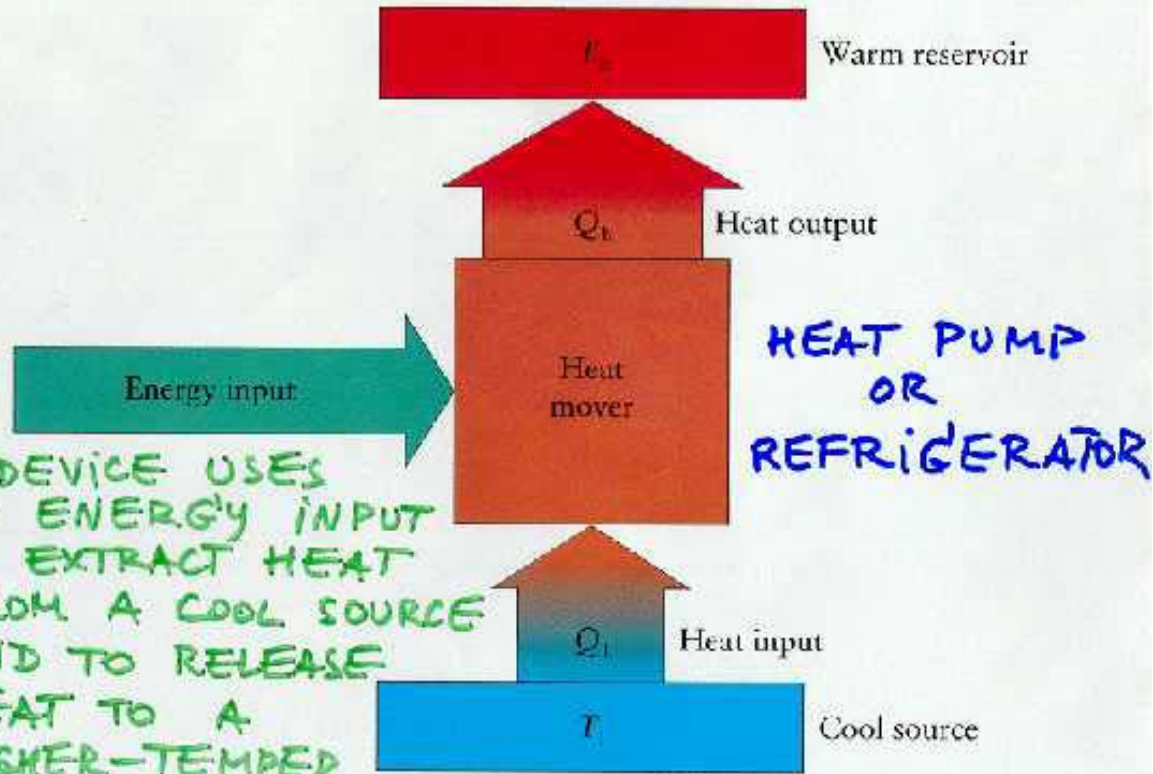
25

Sketch of a Steam-Electric Power Plant



3/)+26.27,28,29,30

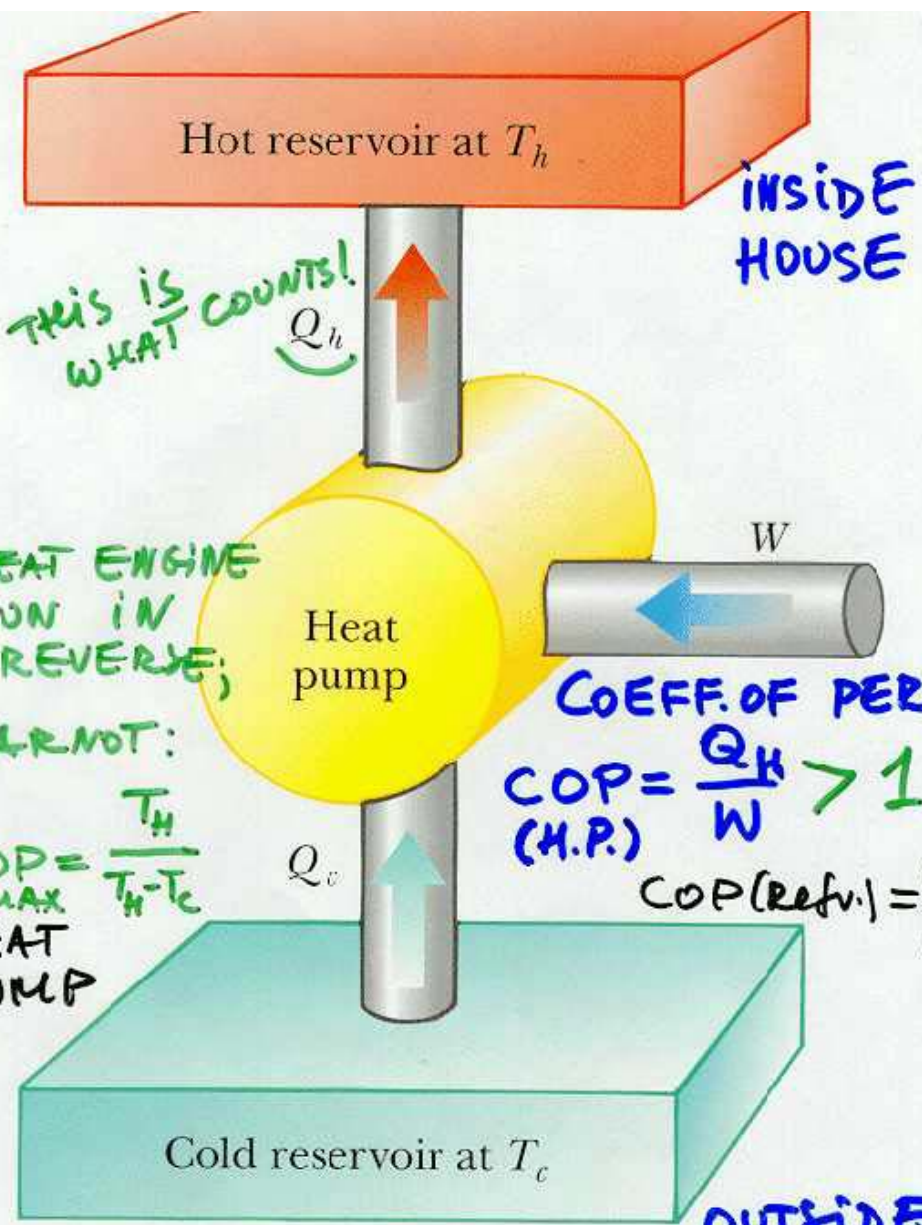
Diagram of a Heat Mover



A DEVICE USES AN ENERGY INPUT TO EXTRACT HEAT FROM A COOL SOURCE AND TO RELEASE HEAT TO A HIGHER-TEMPERATURE RESERVOIR.

Atkins 7th (Figure 5.1)

© 1995 West Publishing Company



THIS IS WHAT COUNTS!
 Q_h

HEAT ENGINE RUN IN REVERSE;

CARNOT:

$$COP = \frac{T_h}{T_h - T_c}$$
 HEAT PUMP

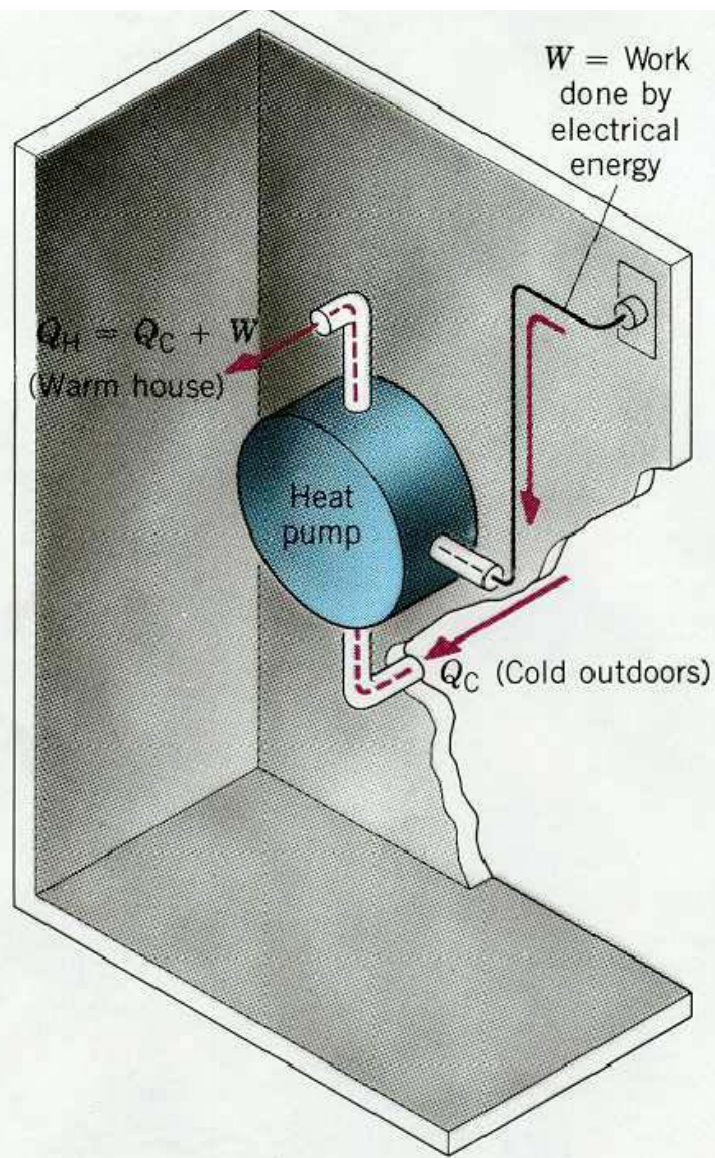
COEFF. OF PERF.

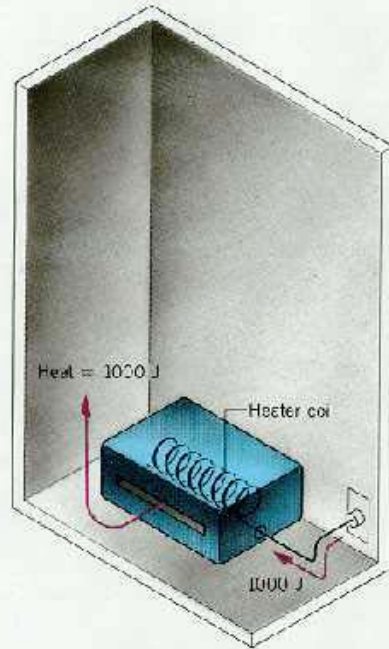
$$COP = \frac{Q_h}{W} > 1$$
 (H.P.)

$$COP(\text{ref.}) = \frac{Q_c}{W}$$

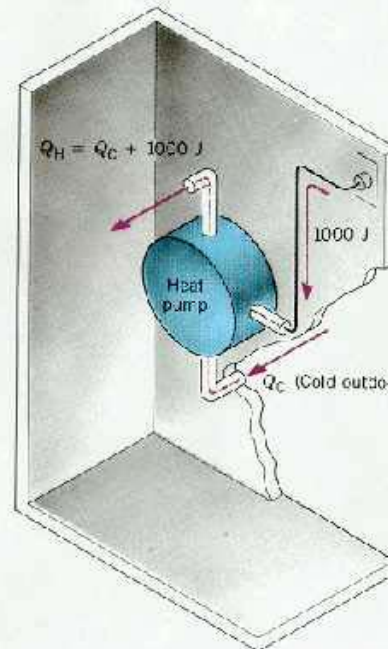
Overhead transparencies to accompany Serway/Faughn: *College Physics, 4/e*
 Figure 62 Text figure 12.12
 Schematic diagram of a heat pump

32)





(a) Conventional electric heating



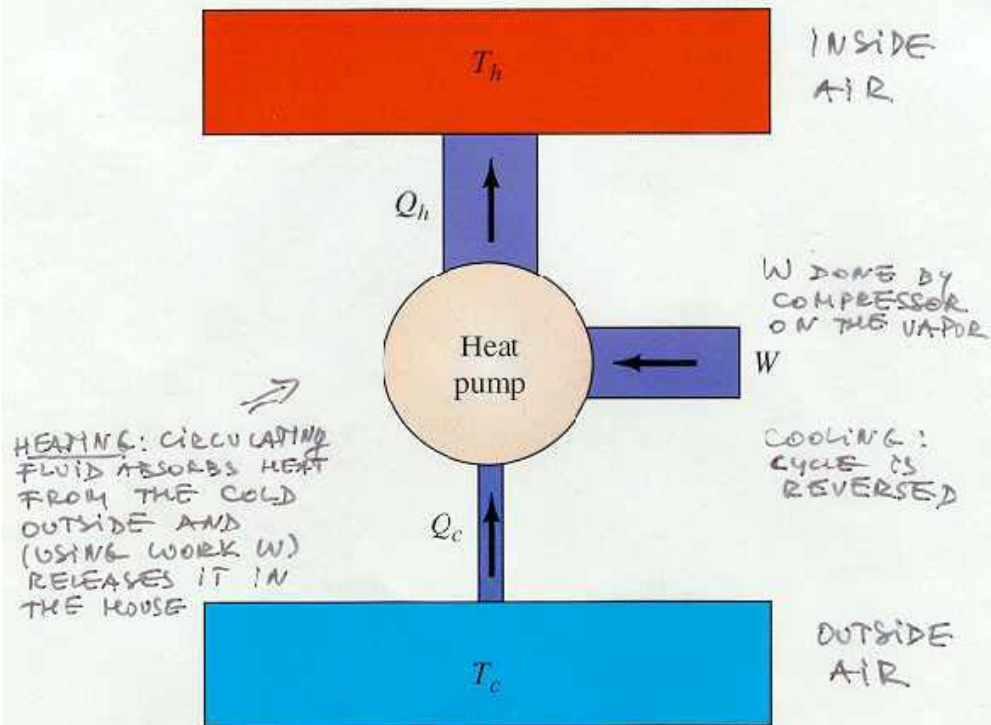
(b) Heat pump

T75 (Figure 20-15) Schematic diagram of a heat pump

COEFF. OF PERFORM.

$$\text{COP}(\text{heat pump}) = \frac{Q_h}{W} \approx 4 \Rightarrow Q_h \approx 4W \quad (\text{regular heater: } Q = W!)$$

$T_c \approx 25^\circ\text{F}$



A REVERSIBLE DEVICE OPERATING BOTH AS A HEATER AND A REFRIGERATOR.

EXAMPLE:

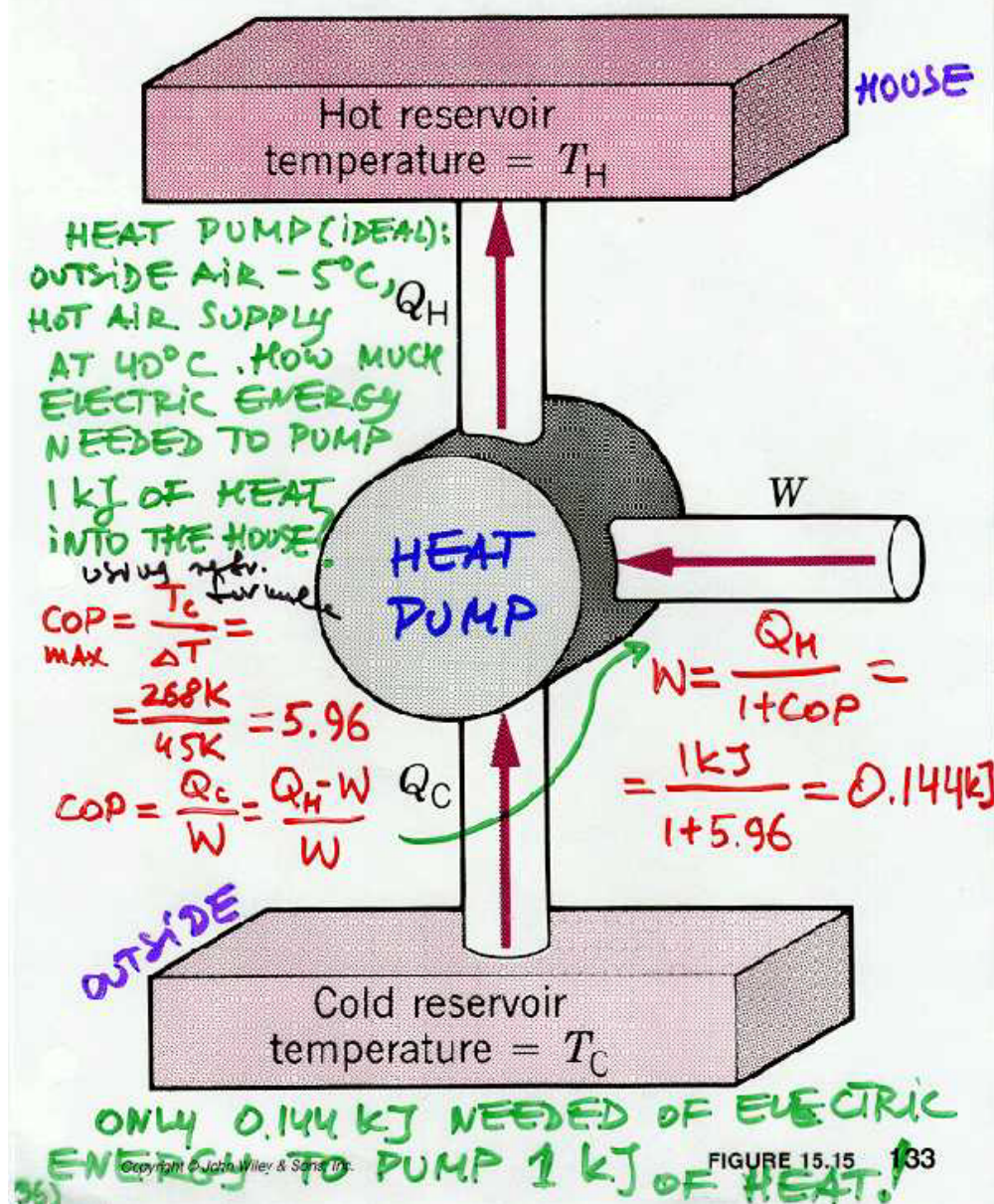
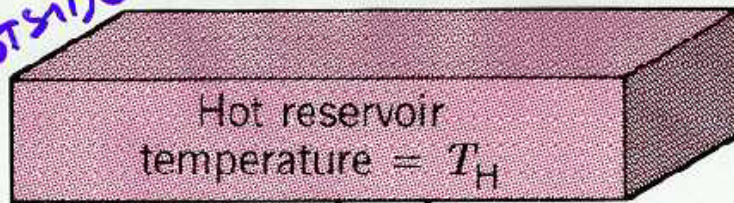
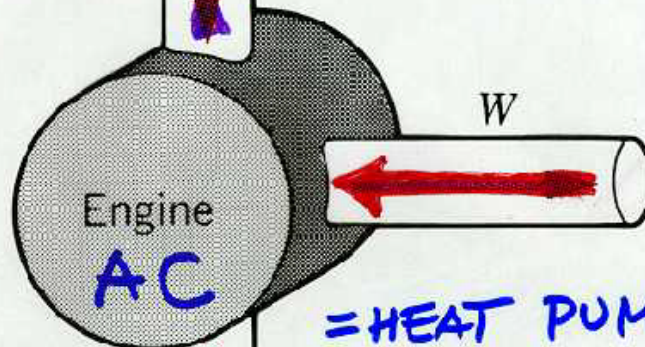


FIGURE 15.15 133

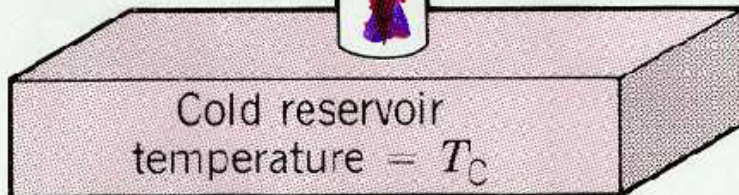
OUTSIDE



AIR
CONDITIONER

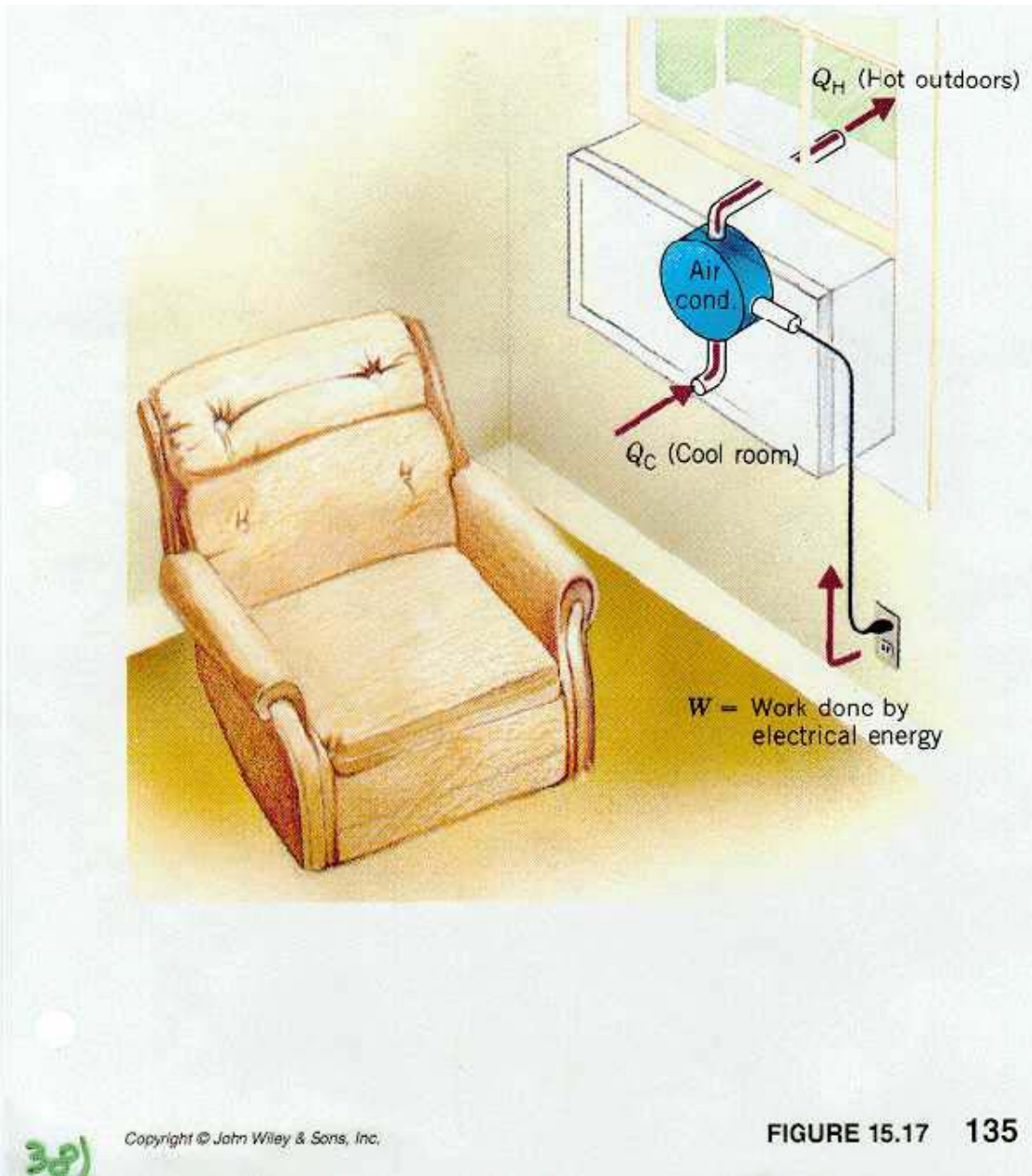


= HEAT PUMP
RUN IN REVERSE



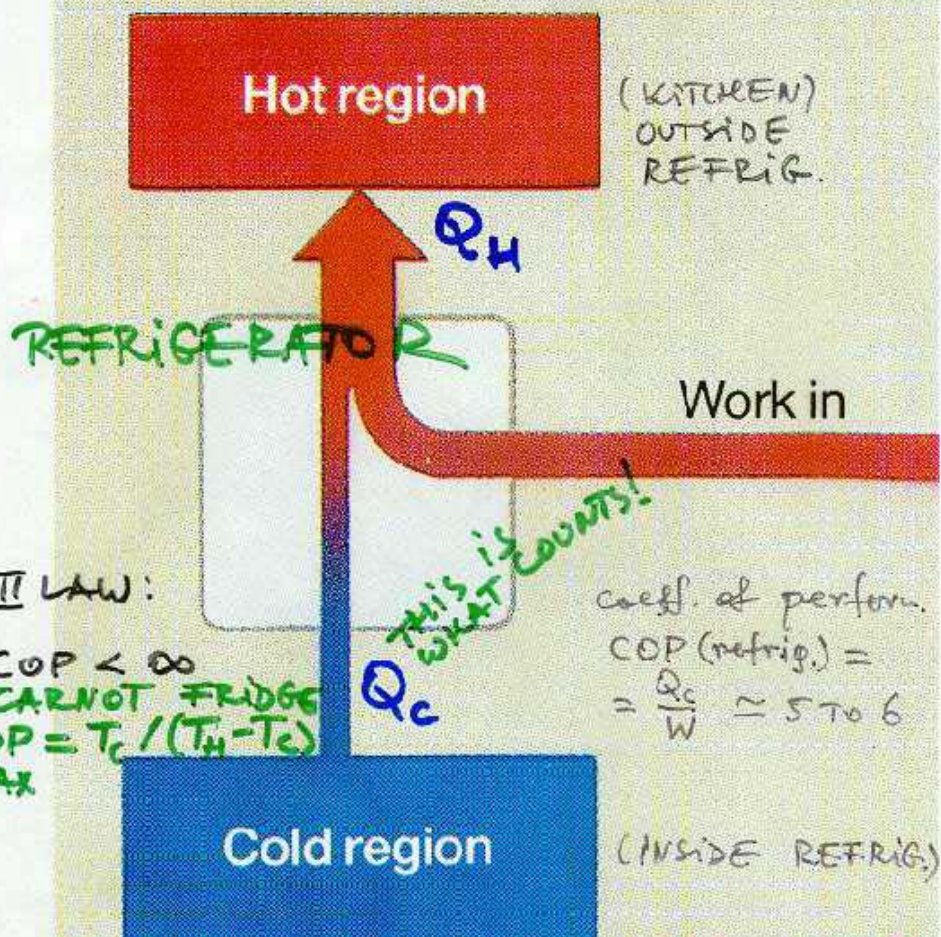
HOUSE

37)



321

REFRIGERATOR USES MECHANICAL WORK TO TRANSFER THERMAL ENERGY FROM A COLDER TO A HOTTER REGION.



II LAW:

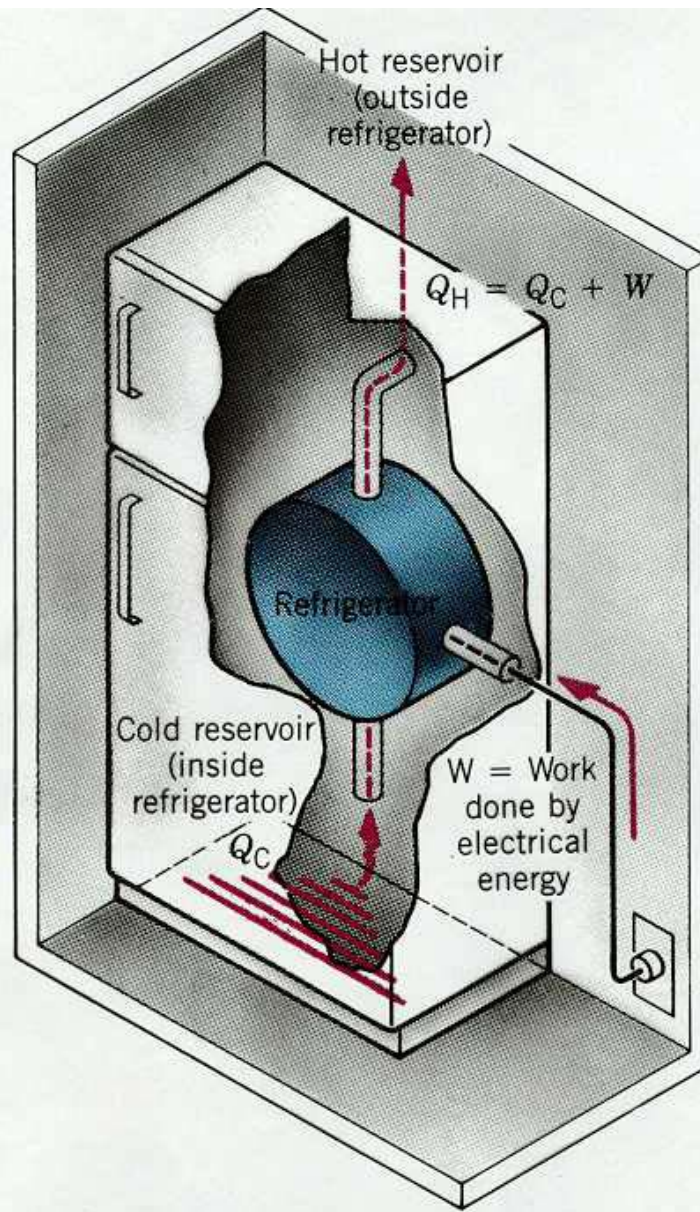
COP < ∞
 CARNOT FRIDGE
 $COP = T_c / (T_h - T_c)$
 MAX

coeff. of perform.
 $COP (refrig.) =$
 $= \frac{Q_c}{W} \approx 5 \text{ TO } 6$

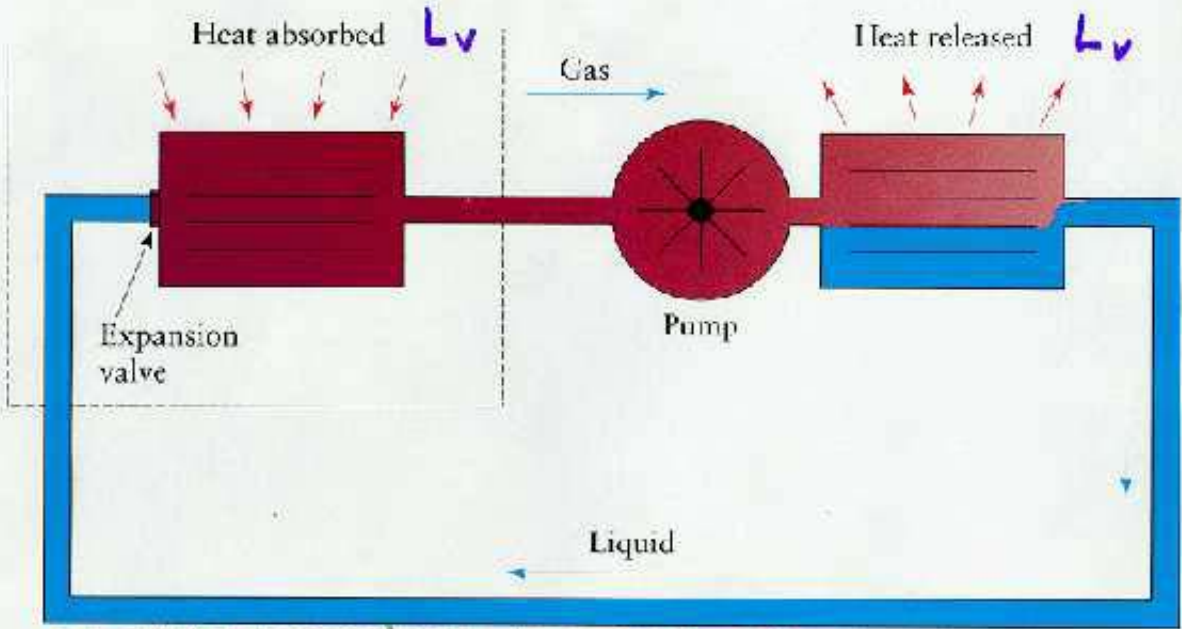
II: A REFRIGERATOR WON'T WORK
 LAW

39)

UNLESS IT'S PLUGGED IN!

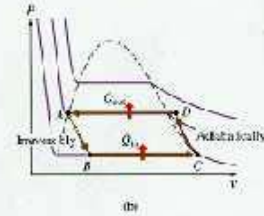
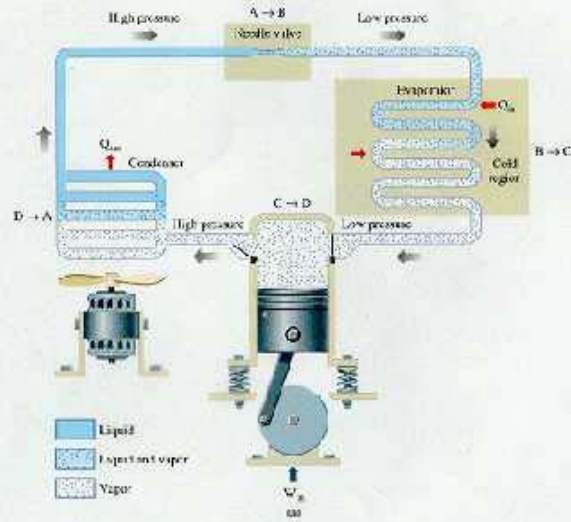


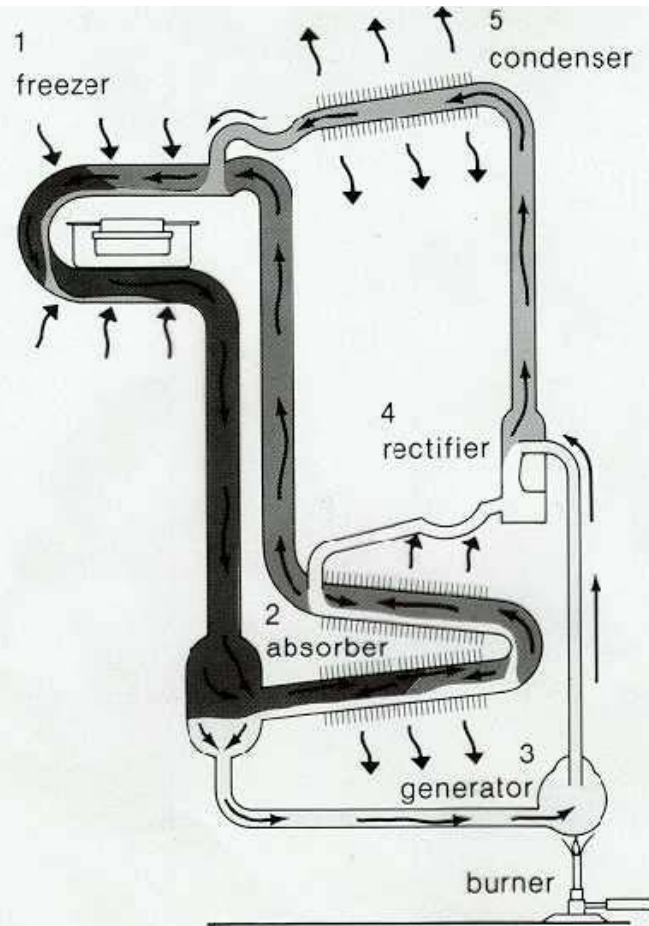
Refrigerator Cooling Cycle









AS THE REFRIGERANT VAPORIZES,
IT ABSORBS HEAT L_v FROM THE
REFRIGERATOR'S INTERIOR;
AS IT CONDENSES, IT RELEASES HEAT TO THE ROOM.

A Refrigeration System





- | | | | |
|---|-------------------|--|----------------------|
|  | water |  | hydrogen |
|  | ammonia and water |  | ammonia and hydrogen |
|  | ammonia |  | heat flow |

100
42'

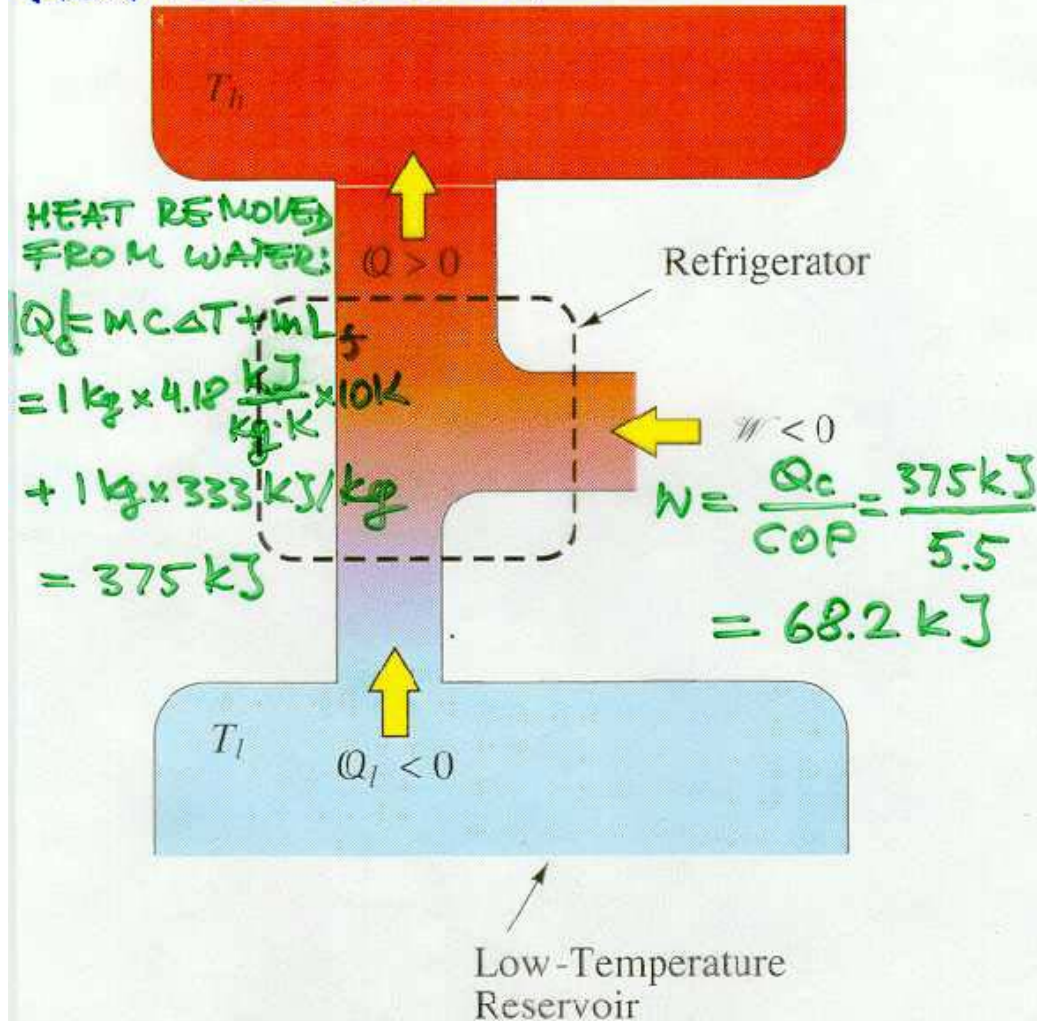
Wilson

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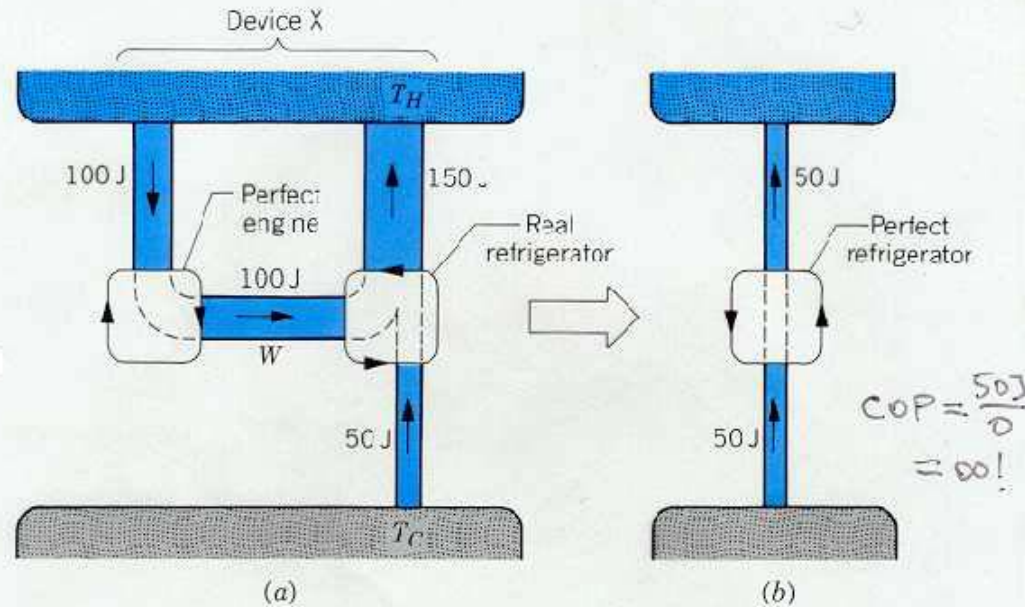
EXAMPLE: GIVEN COP = 5.5,
 HOW MUCH WORK
 IS NEEDED TO
 MAKE ICE CUBES
 FROM 1L OF WATER
 FROM 1L OF WATER AT 10°C?

High-Temperature
 Reservoir

AT 10°C?



A "PERFECT" REFRIGERATOR
 CONSTRUCTED FROM A "PERFECT"
 ENGINE AND A "REAL" REFRIGERATOR

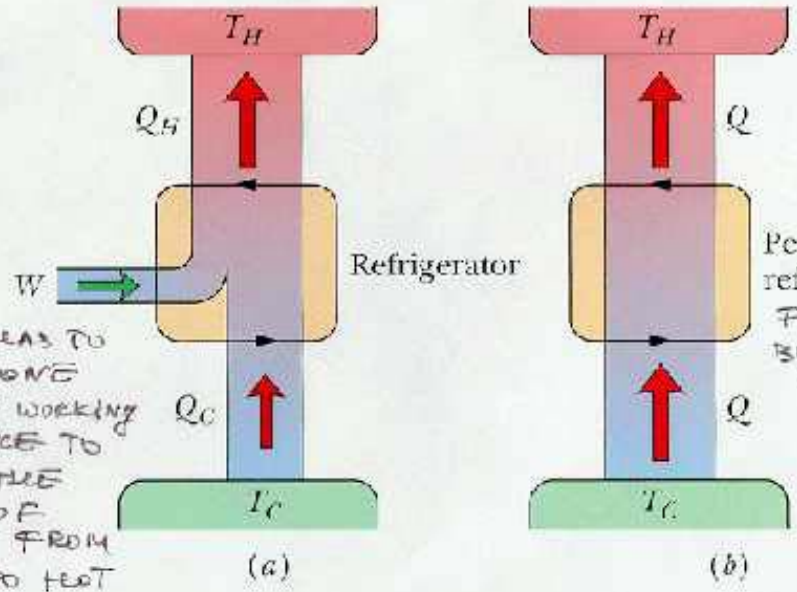


CONCLUSION: PERFECT REFRIGERATOR
 IS IMPOSSIBLE, BECAUSE
 PERFECT ENGINE IS
 IMPOSSIBLE.

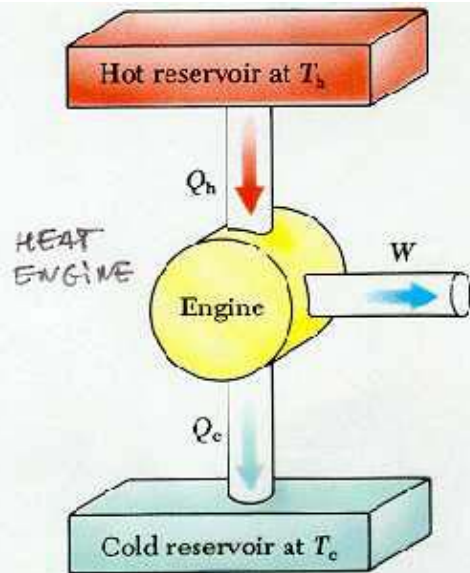
A "perfect" refrigerator constructed from a "perfect" engine and a "real" refrigerator.

ALTERNATIVE FORMULATION OF THE II LAW:
THE CYCLIC MACHINE TRANSFERRING HEAT FROM COLD TO HOT WITHOUT ANY OTHER EFFECTS (LIKE W) IS IMPOSSIBLE

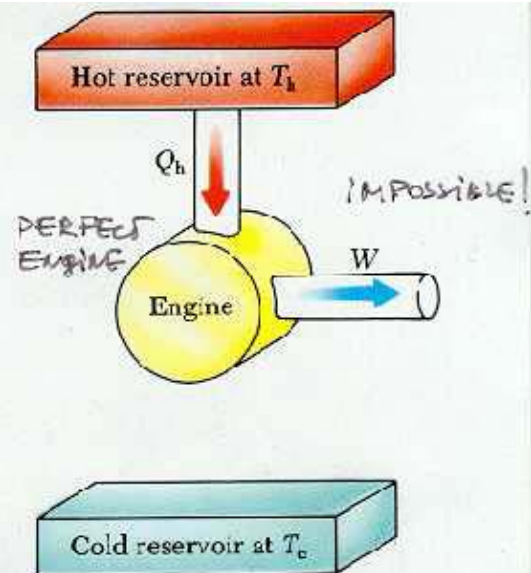
WORK HAS TO BE DONE ON THE WORKING SUBSTANCE TO FORCE THE FLOW OF HEAT FROM COLD TO HOT



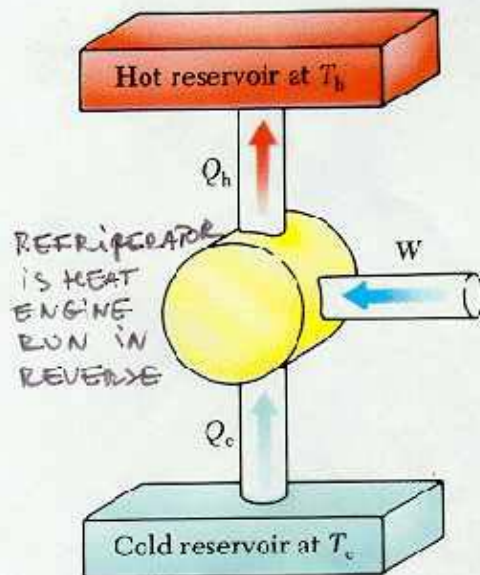
Perfect refrigerator - FORBIDDEN BY II LAW



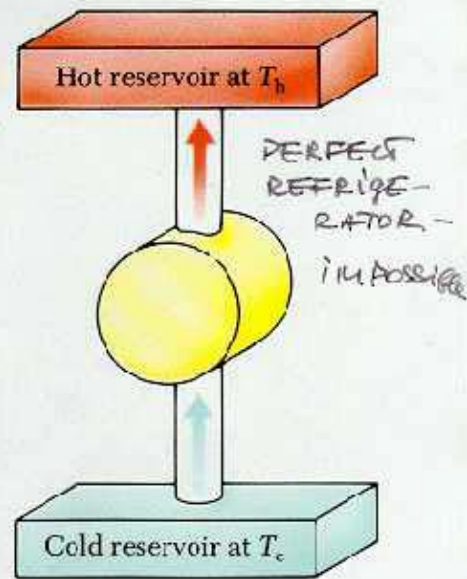
Heat engine



The impossible engine



Refrigerator



Impossible refrigerator

LM

ENTROPY

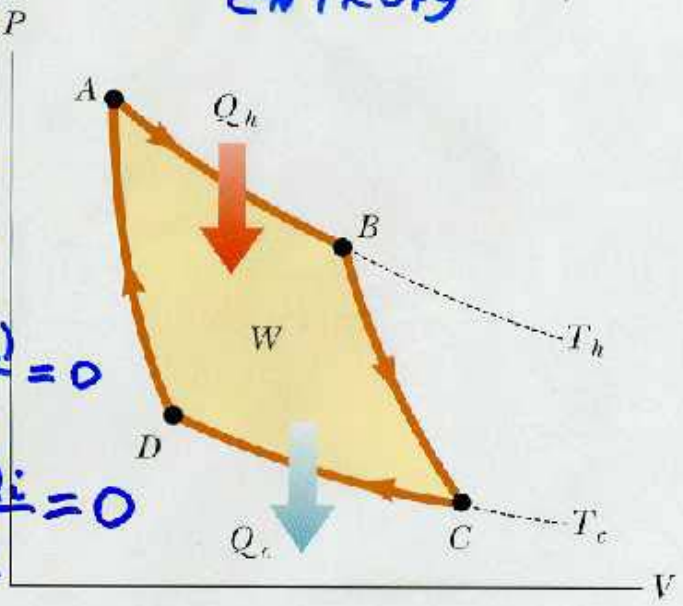
CARNOT
CYCLE:

$$\frac{Q_c}{T_c} = \frac{Q_h}{T_h}$$

OR

$$\frac{Q_h}{T_h} + \frac{(-Q_c)}{T_c} = 0$$

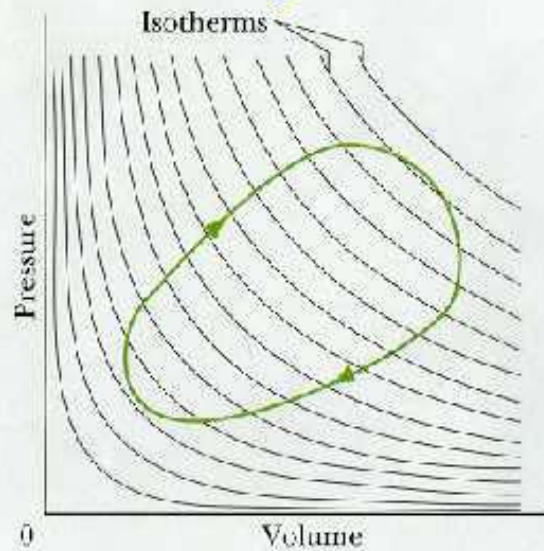
$$\sum_i \frac{\Delta Q_i}{T_i} = 0$$



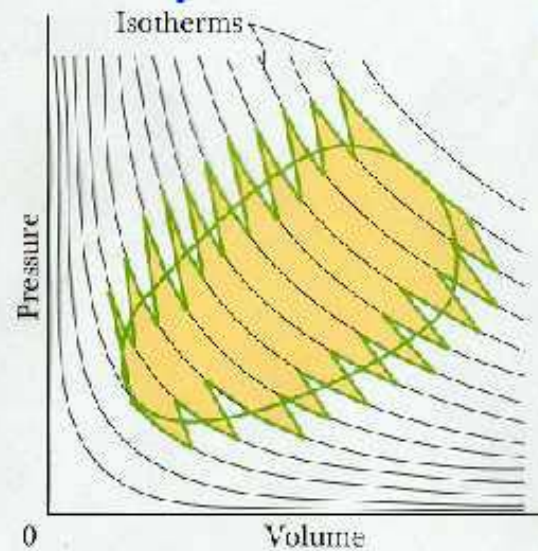
Overhead transparencies to accompany Serway/Jaughn: *College Physics*, 4e
Figure 61 Text figure 12.11
The P-V diagram for the Carnot cycle

ANY REVERSIBLE CYCLE:

$$\sum_i \frac{\Delta Q_i}{T_i} = 0 \Rightarrow \oint \frac{dQ}{T} = 0$$



(a)

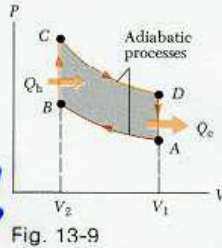


(b)

A CYCLIC REVERSIBLE PROCESS AS A SERIES OF CARNOT CYCLES.

ANALOG: $\oint \vec{F} \cdot d\vec{s} = 0 \Rightarrow$ EXISTS
 POTENT. ENERGY: $\Delta U = - \int_A^B \vec{F} \cdot d\vec{s}$

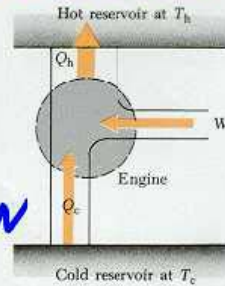
HERE: STATE
 FUNCTION
 $S \equiv$ ENTROPY,



$$\Delta S = \int_A^B \frac{dQ}{T} \quad \Delta S = S_B - S_A$$

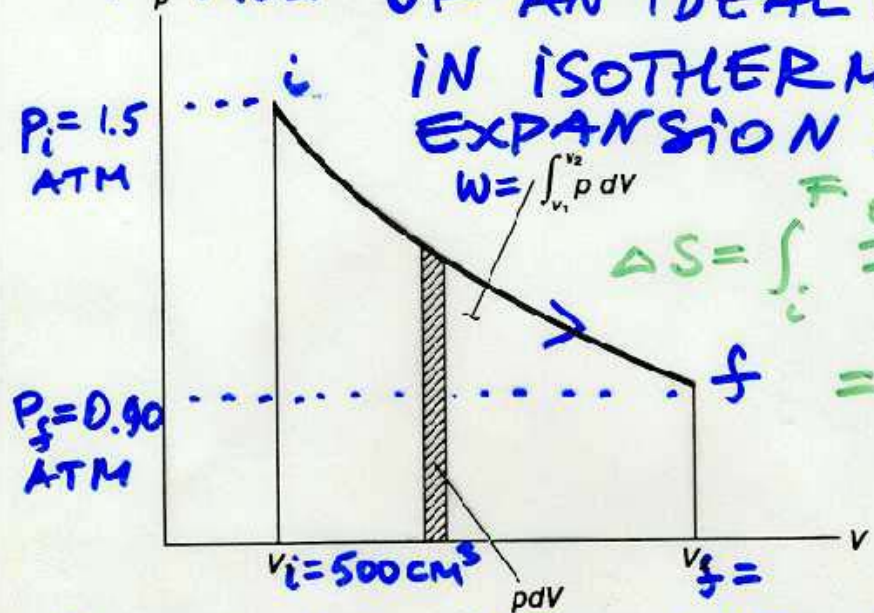
FOR A REVERSIBLE PATH

ENTROPY
 DEPENDS
 ONLY ON A
 POSITION ON
 THE P-V
 DIAGRAM, SO ΔS IS
 PATH- INDEPENDENT.



EXAMPLE: CALCULATE THE ENTROPY CHANGE OF 1 MOL OF AN IDEAL GAS

IN ISOTHERMAL EXPANSION:



$$\Delta S = \int_i^f \frac{dQ}{T} = \frac{Q}{T}$$

I LAW: $dQ = dW + dU = dW$

$Q = W = \int p dv = nRT \int \frac{dv}{v} = nRT \ln \frac{V_f}{V_i}$

$\Delta S = \frac{Q}{T} = -nR \ln \frac{P_f}{P_i} = -(1 \text{ mol}) \times 8.3 \text{ mol} \cdot \text{K} \times \ln (0.90/1.50) = 4.2 \frac{\text{J}}{\text{K}}$

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$\Delta S = 4.2 \text{ J/K}$

50

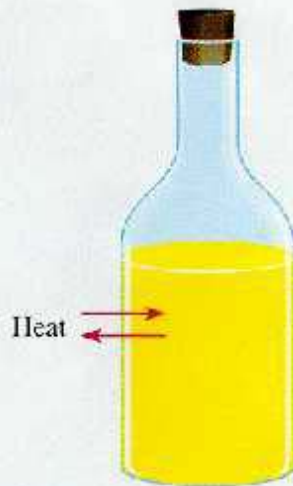
15

OPEN SYSTEM
Water vapor



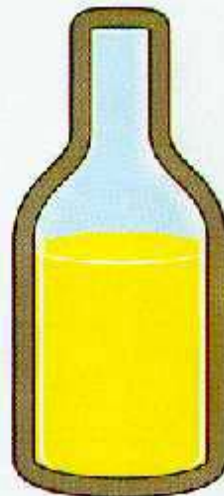
(a)

CLOSED SYSTEM



(b)

"UNIVERSE"
ISOLATED SYSTEM



(c)

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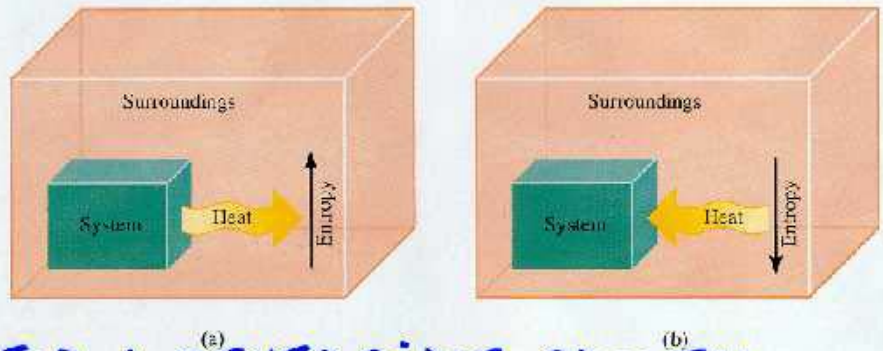
FI

25

ENTROPY OF "UNIVERSE" =
= ENTROPY OF SURROUNDINGS AND SYSTEM

178

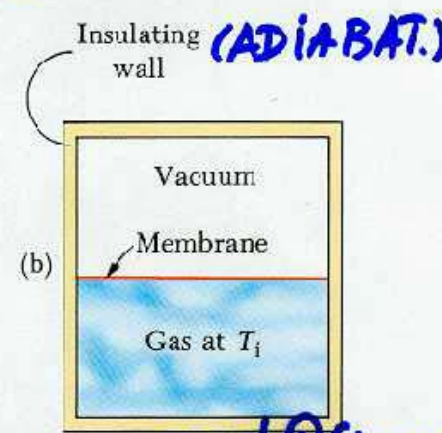
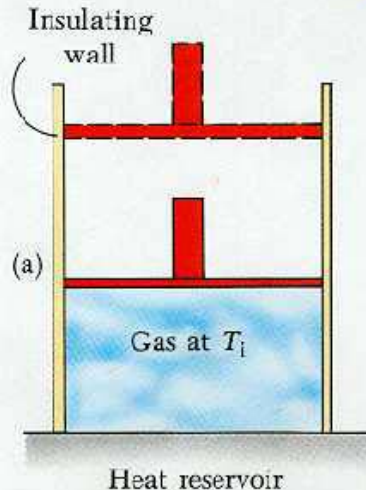
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(a) FOR A REVERSIBLE PROCESS
 $T_{sys} = T_{surr}$, AND $\Delta S_{sys} = \frac{Q}{T}$,
 $\Delta S_{surr} = + Q/T$
 ΔS (ISOLATED SYSTEM) = 0 FOR REVERSIBLE PROCESS

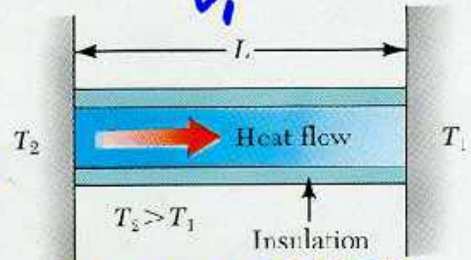
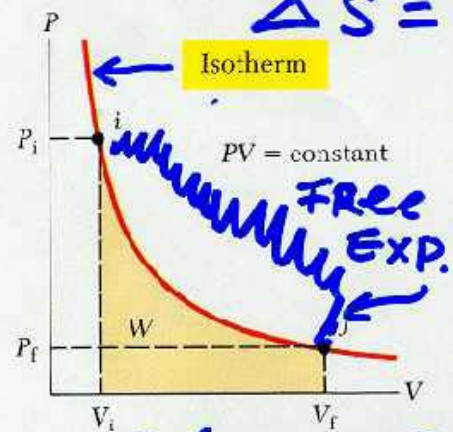
Figure 17-1

FREE EXPANSION OF AN IDEAL GAS - IRREVERSIBLE



$$\Delta S = \int \frac{dQ(\text{rev.})}{T}$$

ISOTHERMAL
 SAME i, f STATES - SAME
 $\Delta S = nR \ln \frac{V_f}{V_i} > 0$



FOR IRREV. PROCESS:
 $\Delta S (\text{ISOLATED SYSTEM}) > 0$

IN GENERAL:
 REVERSIBLE
 PROCESS:
 $\Delta S(\text{UNIVERSE}) = 0$

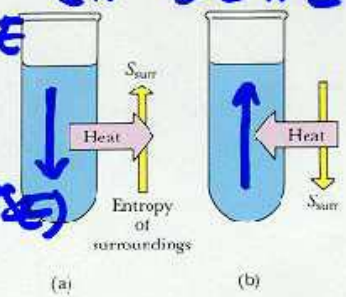


FIGURE 16.13

IRREVERS.
 PROCESS:
 $\Delta S(\text{UNIVERSE}) > 0$

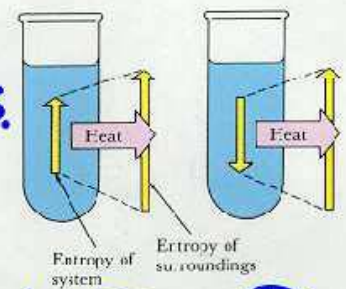


FIGURE 16.14

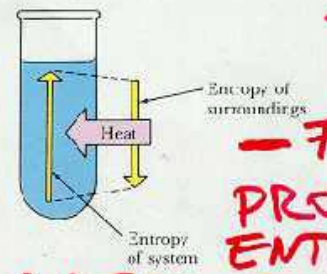
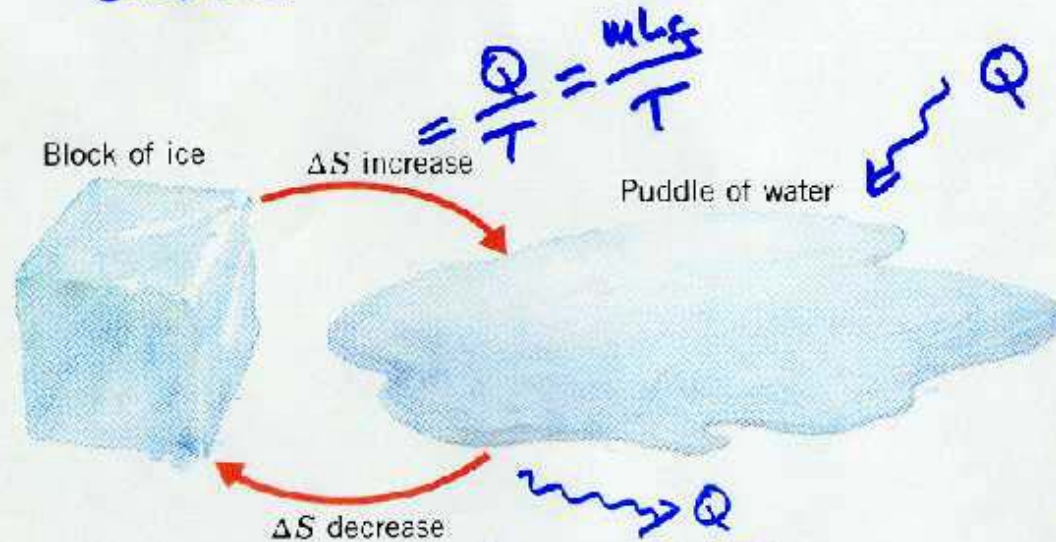


FIGURE 16.15

II LAW:
 $\Delta S \geq 0$
 - FOR ANY
 PROCESS,
 ENTROPY OF

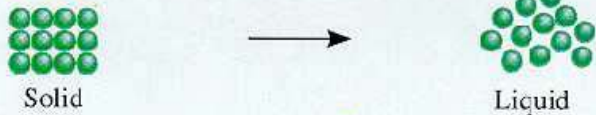
THE UNIVERSE
 NEVER DECREASES

ORDER AND DISORDER

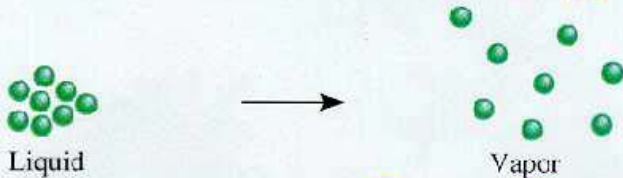


HEAT FLOW INTO THE
SYSTEM INCREASES
ENTROPY AND DISORDER

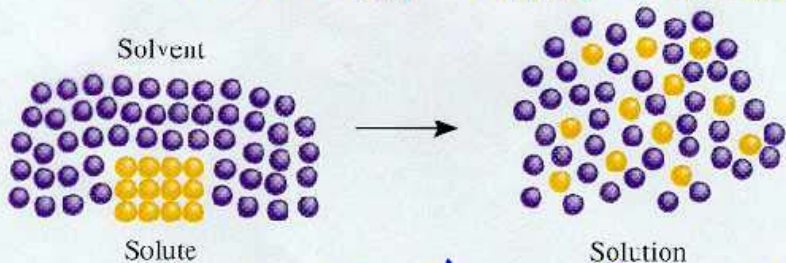
176 THE PROCESSES THAT LEAD TO AN INCREASE IN ENTROPY OF THE SYSTEM Figure 19.2



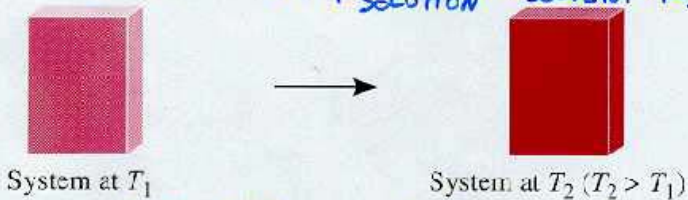
MELTING: (a) $S_{LIQUID} > S_{SOLID}$



VAPORIZATION: (b) $S_{VAPOR} > S_{LIQUID}$



DISSOLVING: (c) $S_{SOLUTION} > S_{SOLVENT} + S_{SOLUTE}$



HEATING: (d) $S(T_2) > S(T_1)$

$\Delta S = \int \frac{dq}{T} = mc \int \frac{dT}{T} = mc \ln(T_2/T_1)$

ALL IRREVERSIBLE PROCESSES
MOVE THE SYSTEM PLUS ITS SUR-
ROUNDINGS TOWARD A LESS ORDERED
STATE:

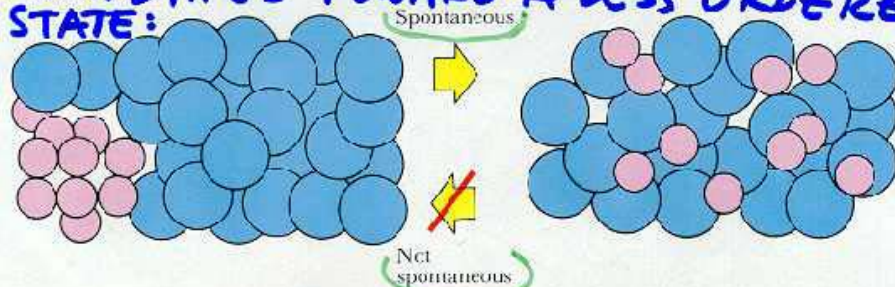
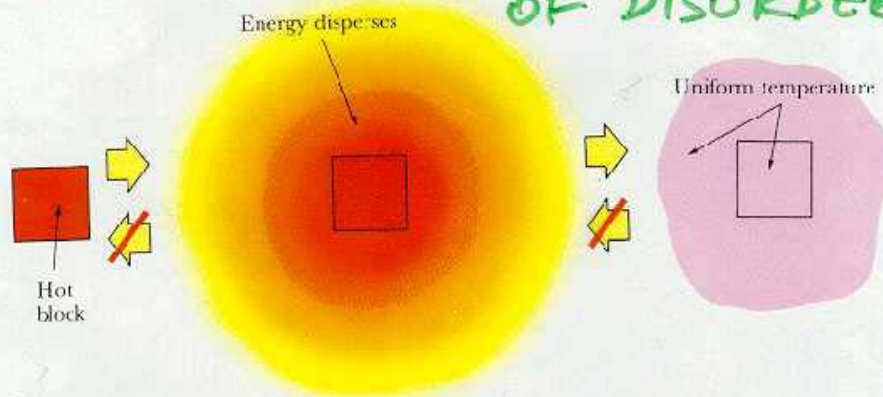


FIGURE 11.18

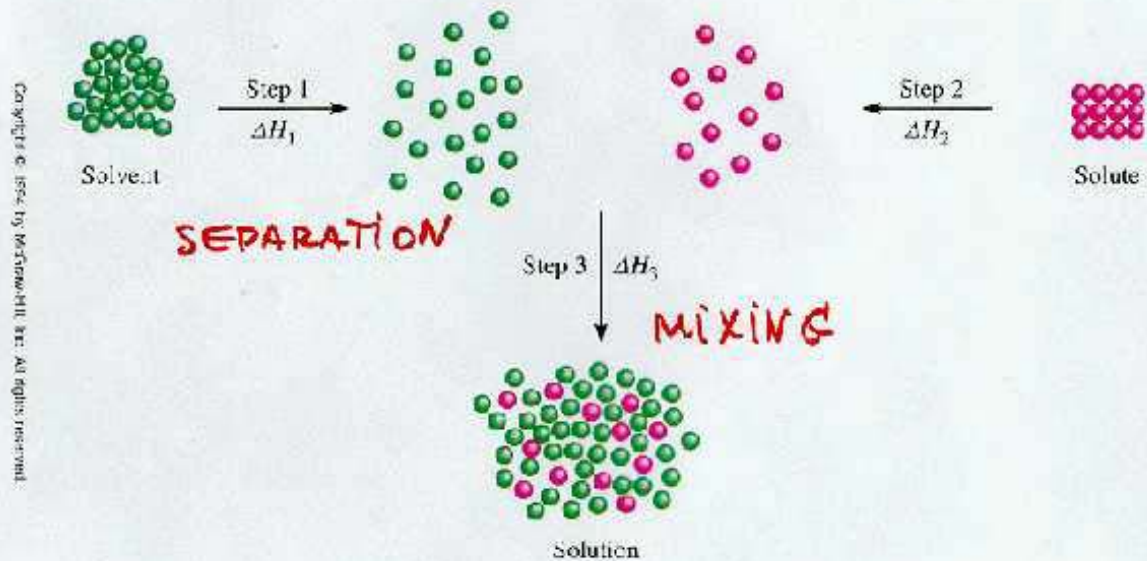
ENTROPY AND MIXING
ENTROPY IS A MEASURE
OF DISORDER



ENTROPY AND TEMPERATURE

FIGURE 11.19

THE SOLUTION PROCESS



$S = k \ln W$
 $k = \frac{R}{N_A} = 1.38 \times 10^{-23} \text{ J/K}$
 $S = k \ln 1$
 $S = 0$

BOLTZMANN
 CONSTANT,
 W-PROBA-
 BILITY,
 OR
 NUMBER
 OF ARRAN-
 GEMENTS

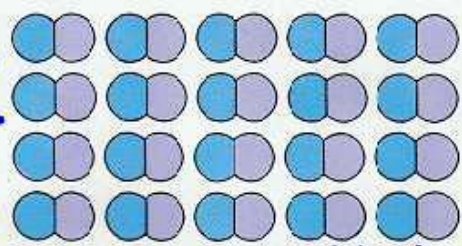


FIGURE 15.7

$N=1$

PERFECT ORDERING
AT $T=0$



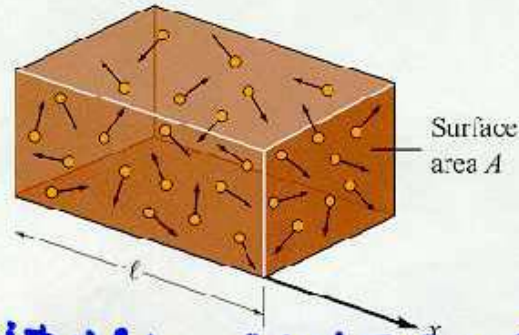
FIGURE 15.8

RANDOM ORDERING
AT $T=0$

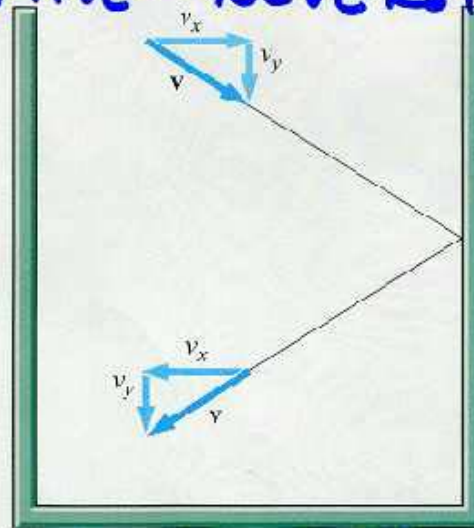
20 MOLECULES, 2 ORIENT.
 FOR EACH, $W = 2 \times 2 \times 2 \dots = 2^{20}$

$S = k \ln 2^{20} = 20k \ln 2 = 1.9 \times 10^{-22} \text{ J/K}$

ENTROPY AND ARROW OF TIME



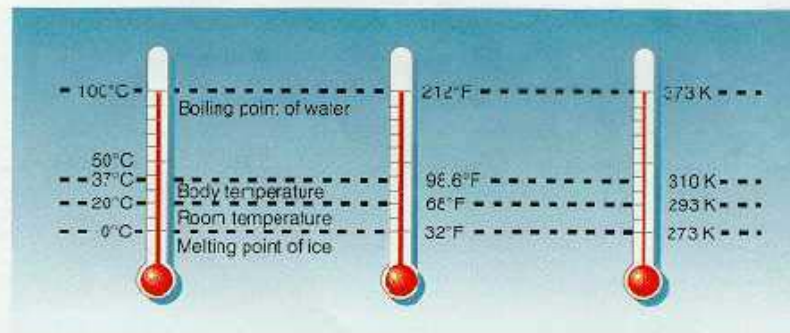
INDIVIDUAL MOLECULES MOVE
IN A TIME-REVERSIBLE WAY



-NO PREFERRED DIRECTION
OF TIME

ARROW OF TIME
MORE ORDER \rightarrow MORE DISORDER
SPONTANEOUSLY!
LESS ENTROPY \rightarrow MORE ENTROPY
IN ISOLATED SYSTEM

REASON: STATISTICAL -
COLLISIONS BETWEEN MOLECULES
LEAD TO MORE DISORDERED
SITUATIONS



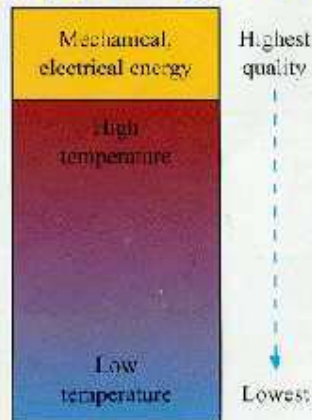
(a) Celsius scale

(b) Fahrenheit scale

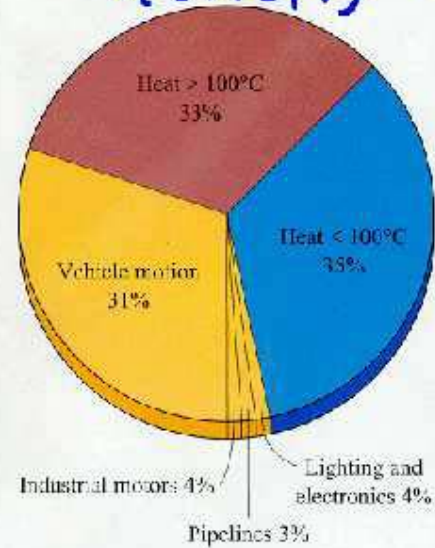
(c) Kelvin or absolute scale

THE ARROW OF TIME EXPRESSES
SIMPLY THE OVERWHELMING
LIKELIHOOD THAT LESS ORDERED
SITUATIONS WILL RESULT

QUALITY OF ENERGY MEASURES THE VERSATILITY OF ENERGY FORMS

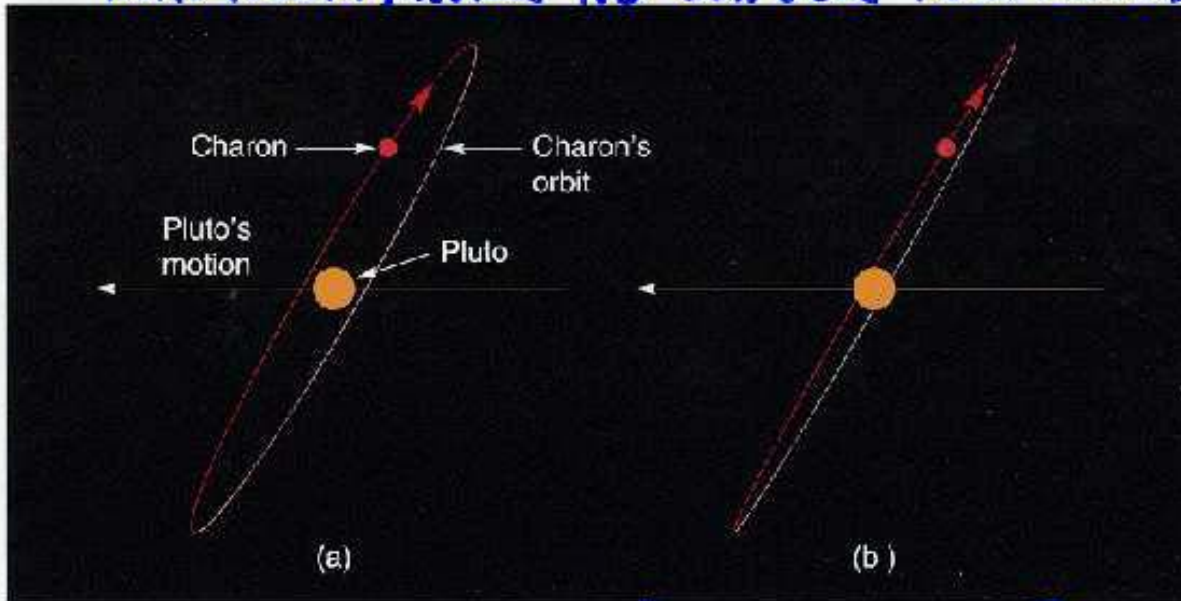


ENERGY USE IN THE U.S. - BY QUALITY



Figures 22-18, 22-19
Physics for Scientists and Engineers, Second Edition
by Richard Wolfson and Jay M. Pasachoff
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HEAT ~~DEATH~~ DEATH OF THE UNCHANGING
UNIVERSE : ALL MATTER REACHES
SAME TEMP., ENTROPY REACHES
MAXIMUM, WORK NO LONGER PERFORMED.



IN ACTUAL EXPANDING UNIVERSE,
HEAT ~~DEATH~~ DEATH UNREALISTIC; UNI-
VERSE MAY EVEN COLLAPSE

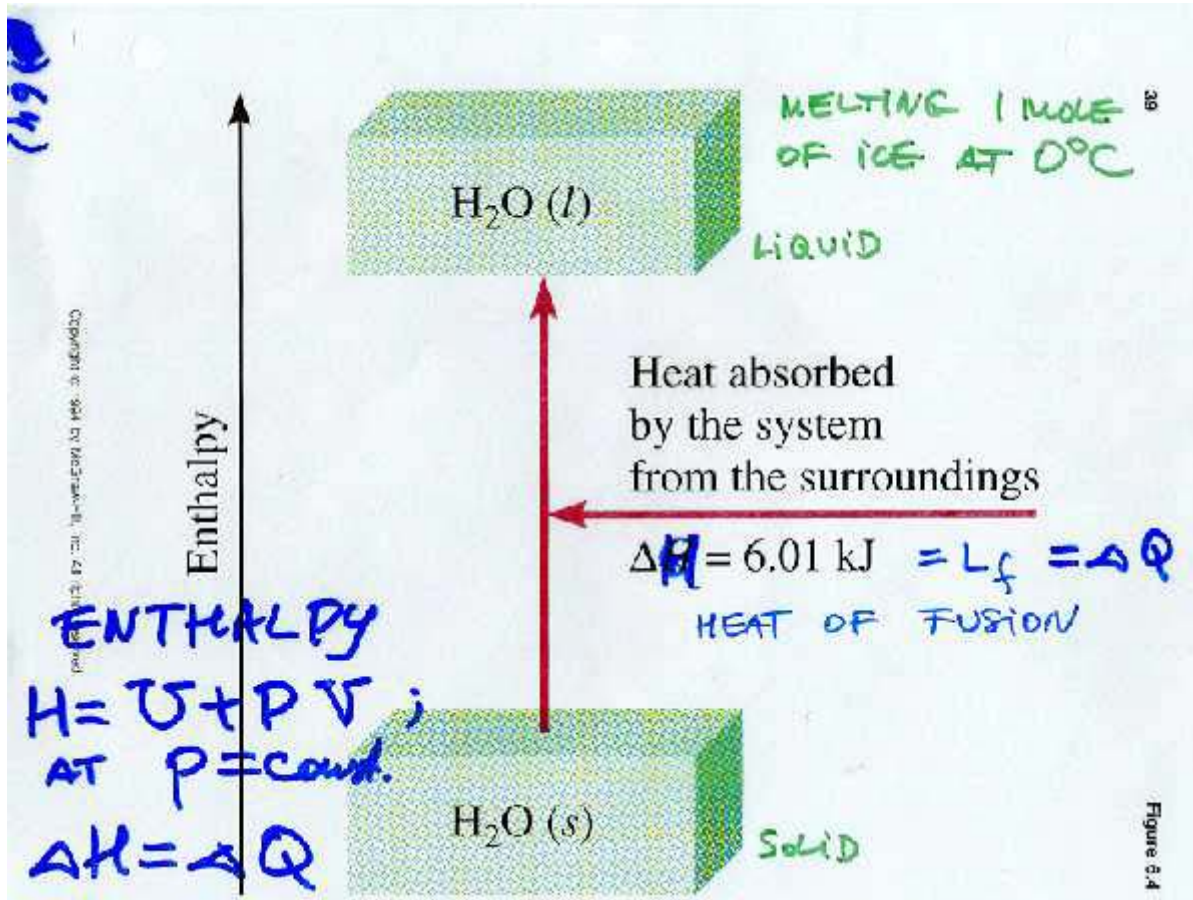


Figure 8.4